

Techno-economics of Biomass Combustion Products in the Synthesis of Effective Low-cost Adsorbents for Carbon Capture

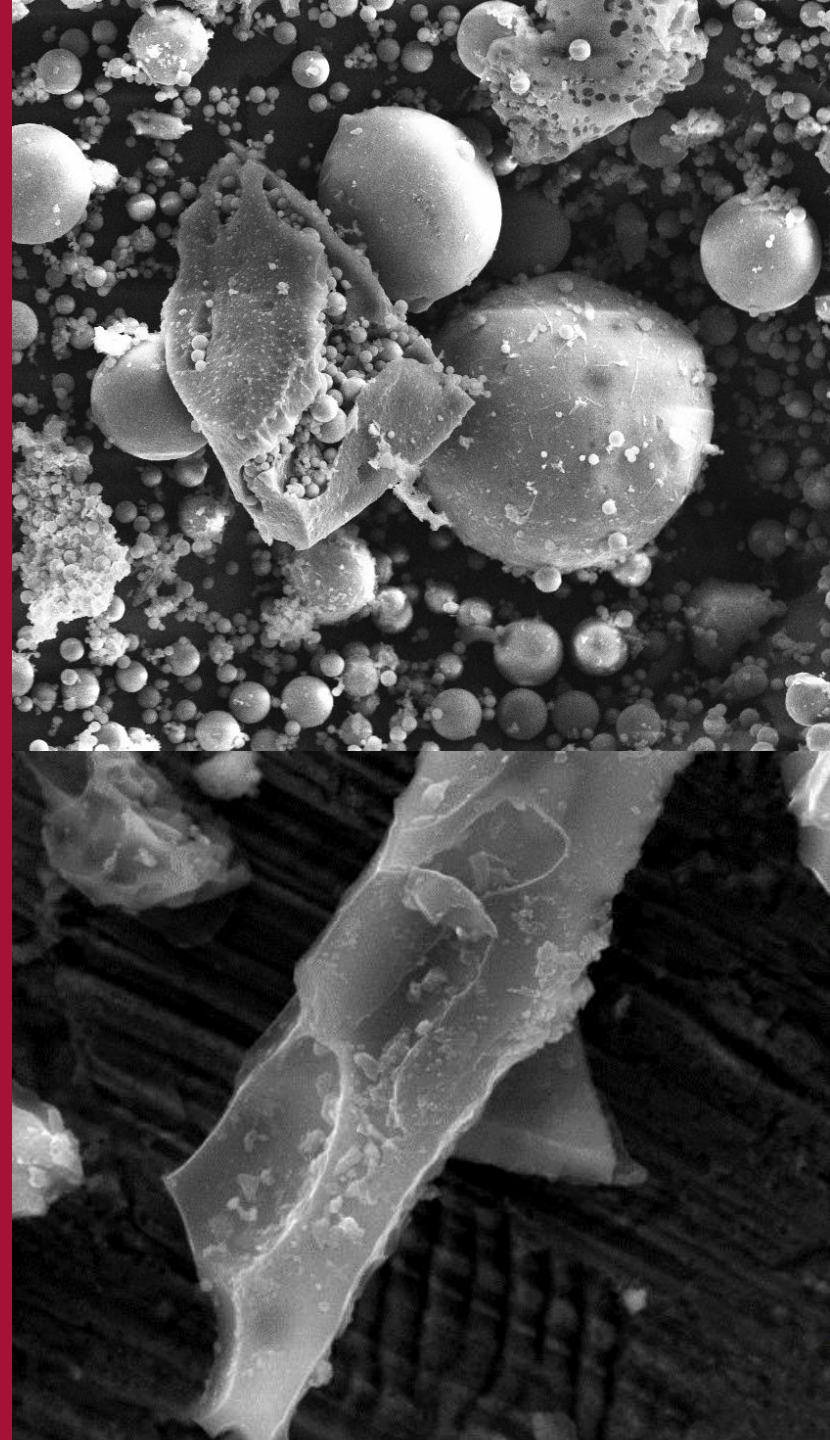
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Proof of Concept

20 May 2022



Fly Ash



Fusion Product



Zeolite



Bottom Ash



Carbon

Experimental Design Conditions

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Factors	Levels		
NaOH/FA Ratio, w/w	1.8	2	2.2
Crystallisation Time, hr	2	6	10
Crystallisation Temperature, °C	50	70	90
Liquid/Solid Ratio, w/w	5	6	7

Zeolite Synthesis

L⁹ Matrix

Carbon Activation

Mixed-level
L²⁵ Matrix

Factors	Levels		
Gas	CO ₂	N ₂	
Activation Time, min	30	50	70
Activation Temperature, °C	700	800	900
Flow Rate, mL/min	100	200	300
Ramp Rate, °C/min	5	15	25

Zeolite Optimisation

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Factors	Levels		
NaOH/FA Ratio, w/w			2.2
Crystallisation Time, hr			10
Crystallisation Temperature, °C			90
Liquid/Solid Ratio, w/w	5		

Optimum Zeolite

Adsorption Capacity at 50 °C
under 50 mL/min pure CO₂

1.65 mmol/g

Factors	Conditions
NaOH/FA Ratio, w/w	1.6
Crystallisation Time, hr	4
Crystallisation Temperature, °C	90
Liquid/Solid Ratio, w/w	7.69

”Proof of Concept” Zeolite

Adsorption Capacity at 50 °C
under 50 mL/min pure CO₂

0.825 mmol/g

Carbon Optimisation – Step 1

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Factors	Significance
Gas	1
Activation Time, min	Statistically Insignificant
Activation Temperature, °C	2
Flow Rate, mL/min	Statistically Insignificant
Ramp Rate, °C/min	3

$R^2 = 0.936$

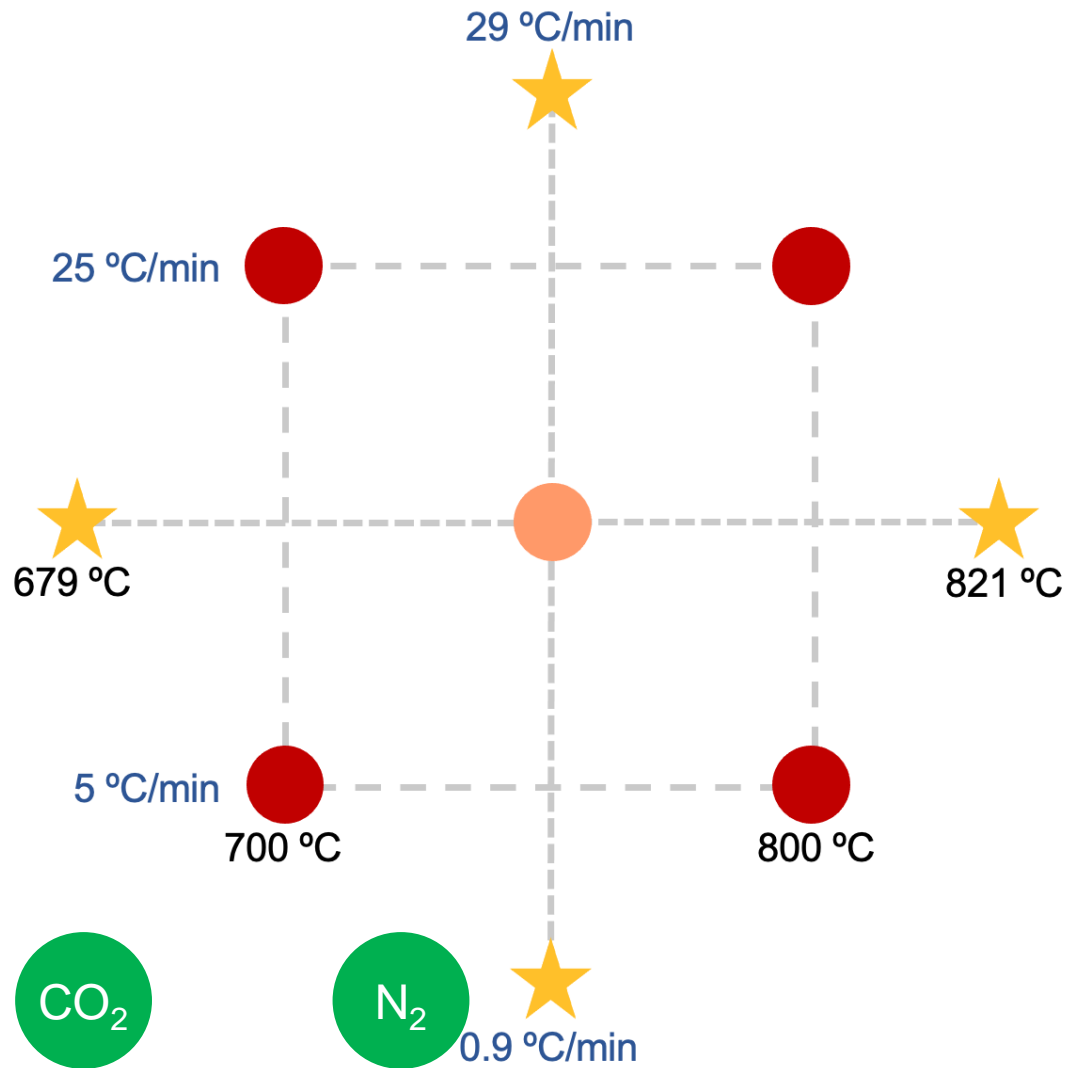
Reverse Boudouard Reaction



Activation Temperature, °C	Uptake at 50 °C, mmol/g	Yield, %
700	~ 0.6	~ 52
800	~ 0.3	~ 25
900	0	~ 13

Carbon Optimisation – Step 2

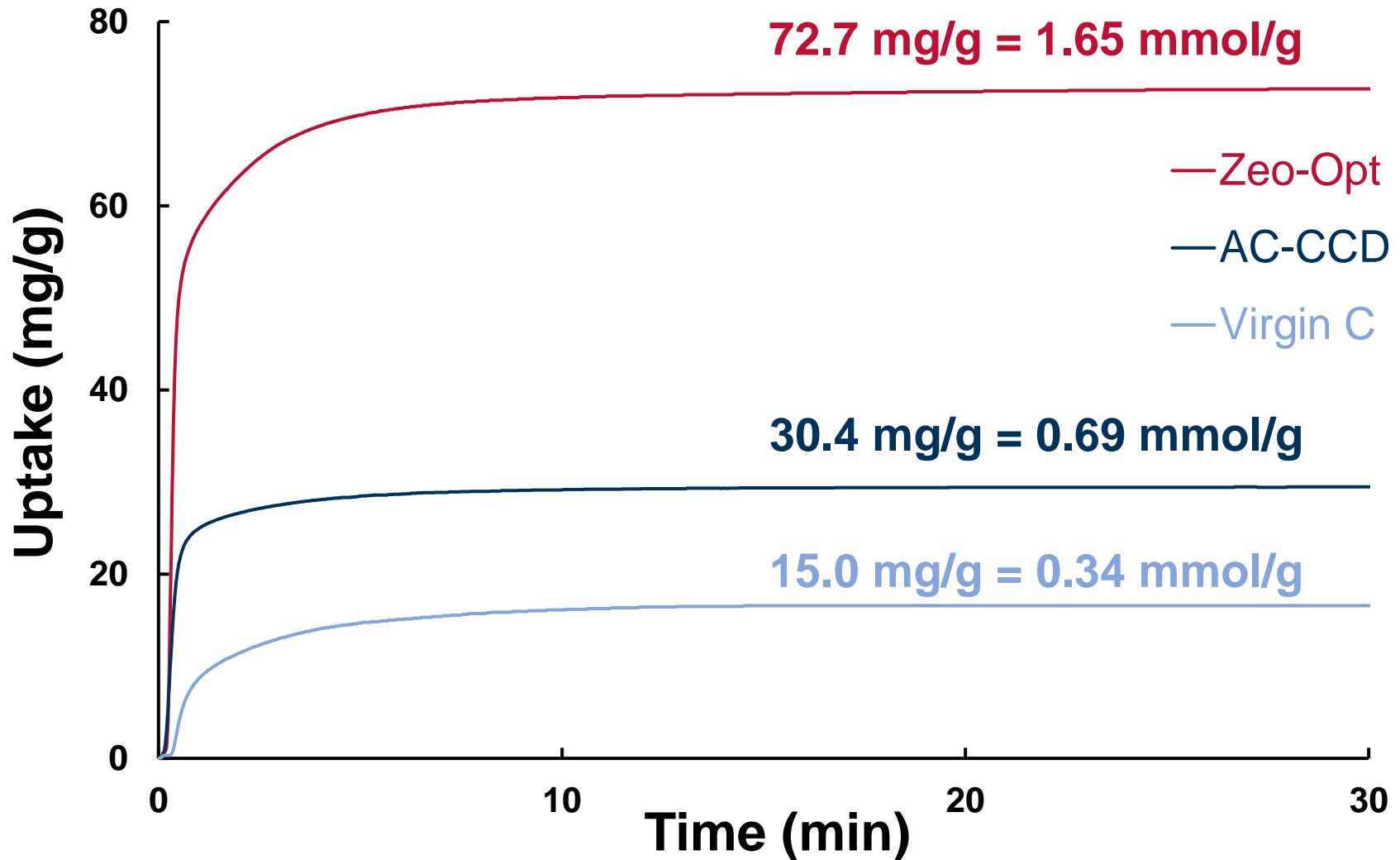
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CO₂ Adsorption Performance

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T = 50 °C; P = 1 atm; C_(CO₂) = 100%



Study in progress, however, some notable points:

- Lack of logistics/transport costs (if deployed *in-situ*)
- Waste valorisation = Minimisation of landfilling costs
 - Increased rates as of 1st April 2022:

- Standard rate = £98.6/tonne
- Lowered rate = £3.15/tonne

BA-derived carbon:

- Reclaimed pulverised biomass (by-product of extraction) could be readily reintroduced into the boiler as fuel, increasing the overall efficiency of the plant or in a stand-alone unit providing the required energy for sorbent regeneration, thus significantly reducing the parasitic load of the capture process.
 - Another reduction in the quantity of waste ash sent to landfill
- Absence of a carbonation step
- Physical activation is cheaper and more eco-friendly than chemical activation
- The captured CO₂ could be recycled in the process as the activating gas
- Potentially even lower activation temperature

Published Papers

Petrovic, B.A.; Gorbounov, M.; Masoudi Soltani, S.

- Impact of Surface Functional Groups and Their Introduction Methods on the Mechanisms of CO₂ Adsorption on Porous Carbonaceous Adsorbents
 - > Published in '**Carbon Capture Science & Technology**' journal.
 - > Available online; **DOI: 10.1016/j.ccst.2022.100045**

Under review

- ❑ Synthesis of Nanoporous Type A and X Zeolite Mixtures from Biomass Combustion Fly Ash for Post-Combustion Carbon Capture
- ❑ Development of Nanoporosity on a Biomass Combustion Ash-derived Carbon for CO₂ Adsorption
- ❑ Extraction of Cellulose Nanofibre Layer from Biomass Bottom Ash
- ❑ Technical Review of Experimental Design Techniques in Synthesis and Application of Carbonaceous Adsorbents in Chemical Processes

Acknowledgements

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Engineering and
Physical Sciences
Research Council

Thank you! Q&A



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