

Best Available Techniques for 'Blue' Hydrogen Production with Carbon Capture and Storage

Jane Durling

Senior Advisor – Energy Team

Radioactive Substances and Industry Regulation

02/11/21

Best Available Techniques for 'Blue' Hydrogen Production with Carbon Capture and Storage

- What are BAT – best available techniques?
- BAT guidance
 - When is BAT guidance needed?
 - Criteria for determining BAT
 - Development process
- Summary of Process Inputs/Outputs
- Key points for guidance
 - Configuration Choice
 - Performance
- Next Steps
- Published Guidance
- BAT and the Hydrogen Strategy
- Future guidance
- Questions?

What are BAT?

- ‘Best Available Techniques’ *
 - economically and technically viable techniques
 - best for preventing or minimising emissions and impacts on the environment as a whole

* Directive 2010/75/EU of the European Parliament and of the Council of 24 November 2010 on industrial emissions (integrated pollution prevention and control) (europa.eu)

BAT Guidance

When is BAT guidance needed?

- Where no relevant BAT reference document (BRef)
- Regulator must set permit conditions following Art.14(6)
- Must consider criteria for determining BAT in Annex III
- Permit conditions must protect the environment
 - basic obligations of the operator (Art 11)
 - environmental quality standards (Art.18)
- Encourage emerging techniques (Art. 27)

BAT Guidance

Criteria for determining best available techniques (IED Annex III)

- Available to be implemented – economically/technically viable at scale
- Emissions to air/water/land including heat, vibrations, noise – effects/quantity
- Low waste - maximise recovery/recycling
- Less hazardous substances
- Energy efficiency
- Raw material/water usage
- Prevent/reduce overall impact
- Prevent/minimise consequences of accidents
- Take account of published information – international

BAT Guidance

Development Process

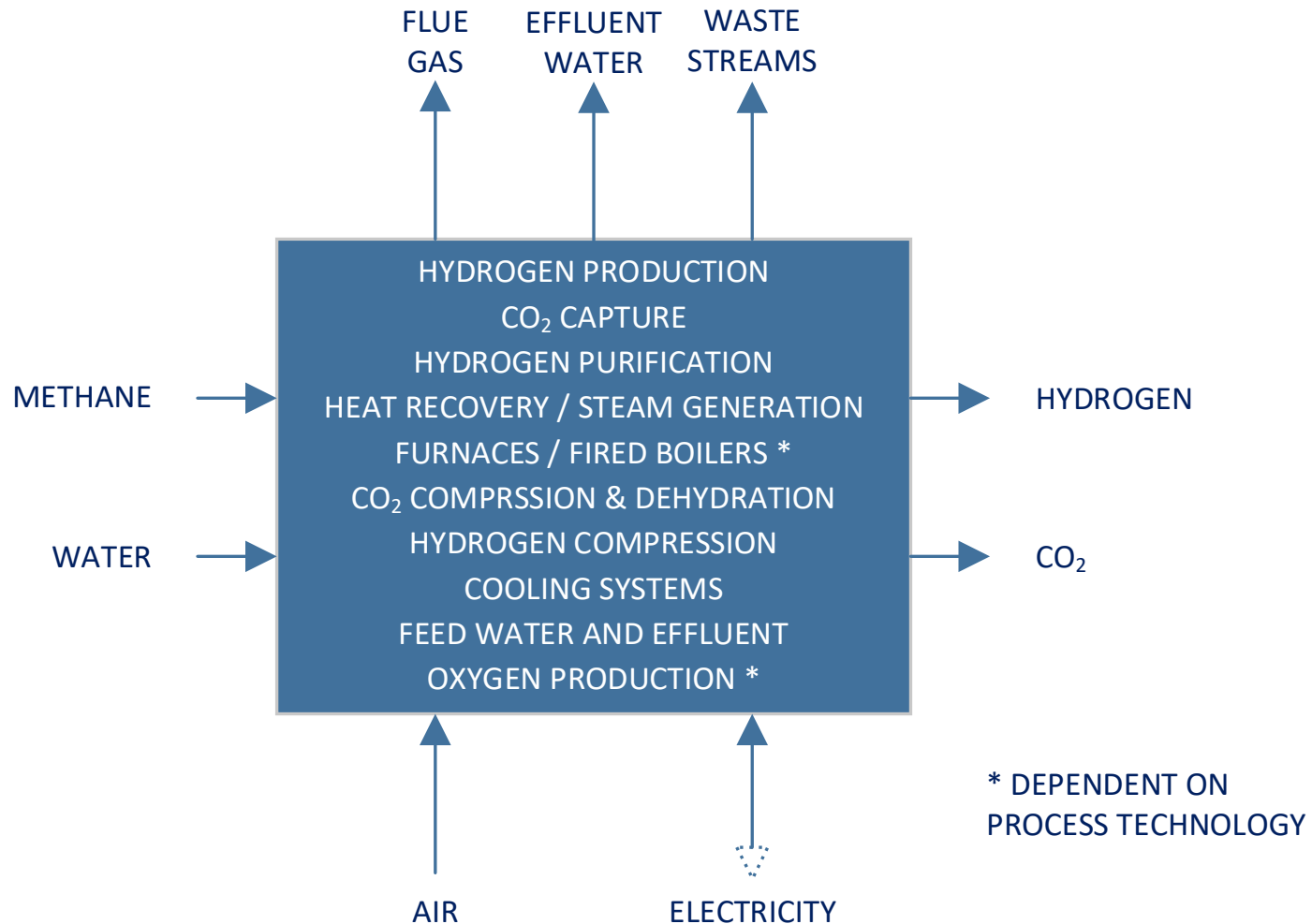
- BAT review informs BAT guidance
- Summarises the evidence for available process options
- Identifies key environmental issues to address & best practice
- In consultation with industry & agreed by UK regulators
- Assists applicants & regulators in the permit process
- Does not set BAT standards or limits
- Permit conditions – generate evidence for future BAT standards

'Blue' Hydrogen Production Technologies Identified

- Steam Methane Reforming (SMR)
- Autothermal Reforming (ATR)
- Gas Heated Reforming (GHR)
e.g. GHR+ATR or GHR+SMR combined
- Partial Oxidation (POX)

* All will need Carbon Capture and Storage (CCS)

Summary of Process inputs/outputs



Key Points for Guidance

– CO₂ Capture Efficiency

- Overall CO₂ Capture Efficiency >95%
 - Feed gas energy conversion
 - Impact on total CO₂ to be captured from process
 - Capture rate
 - Near complete for process CO₂ capture
 - Post combustion capture >95%
 - CH₄, CO and CO₂ left in hydrogen purification tail gas used as fuel
 - Conversion of methane in reforming
 - Conversion of CO in shift reaction
 - Capture of CO₂ from process

Key Points for Guidance – Energy/Process Efficiency

- Energy Efficiency
 - Electrical power requirement
 - Excess HP steam – for power/drives/LP steam
 - Oxygen – additional power demand
- Water
 - availability/quality
 - raw material and cooling
- Feed gas
 - S and higher HC content
- Hydrogen product
 - Inerts
- Carbon dioxide
 - Specification for pipeline/storage
 - Delivery pressure

Key points for Guidance

– Processes with post-combustion capture

- Solvent selection, reflect the balance between CO₂ capture performance, associated energy requirements and potential atmospheric emissions, such as:
 - Energy requirements
 - Reclaiming potential
 - Potential for reaction with contaminants in flue gas, e.g. NO_x removal.
 - Potential atmospheric emissions of solvent and associated degradation products such as nitrosamines and nitramines.
 - Proven performance through operational experience, or test programmes under realistic operating conditions.
- Atmospheric emissions, considering:
 - Emissions of solvent components.
 - Emission of additional substances formed in the CO₂ capture system such as nitrosamines, nitramines and ammonia.
 - Emission of ammonia present in flue gas though slippage from upstream NO_x removal.
 - Formation of further additional substances in the atmosphere from those emissions.

Key Points for Guidance- Emissions to Air

Continuous

- Fired heater / steam boiler flue gas
 - Hydrogen rich / low carbon fuel
 - NO_x formation – potential need for abatement
- Steam vents – e.g. deaerator

During start-up, abnormal conditions

- Flare combustion products
- CO₂ vent from amine regeneration tower

Key Points for Guidance- Emissions to Water

Continuous effluent treatment discharges

- Process condensate
 - Containing e.g. methanol, ammonia, CO₂
 - Downstream of CO shift
 - From CO₂ compression / dehydration regeneration
- From air dehydration in oxygen production
- Boiler blowdown
- Cooling tower blowdown (where appropriate)
- Water purge from amine system
 - From regeneration reflux, containing e.g. methanol
 - From water wash
- Potential for water treatment for reuse

Key Points for Guidance - Waste Streams

- **Liquids**

- Demineralised water production reject stream
- Amine solvent – e.g. from bleed / feed, replacement
- Dehydration solvent – e.g. in case of tri-ethylene glycol dehydration
- Amine reclaimer residue

- **Solids**

- Depleted catalyst material
 - Hydrogenation, reforming, CO shift
- Spent adsorbent materials
 - Gas treatment, dehydration, hydrogen purification
- Solids from amine filtration
- Soot (POX process)

Key Points for Guidance - Monitoring

- Emissions to Air – NO_x , CO , SO_2 , NH_3 , amines/degradation products
- Emissions to Water – NH_3 , amines, methanol
- CO_2 capture performance
- Process performance – energy efficiency, solvent performance

Next Steps

- BAT review complete.
- BAT guidance subject to final regulatory confirmation
- Guidance to be published on .gov.uk
- BAT review will be referenced
- BAT review available on request

Published BAT Guidance and BAT Review for Post Combustion CCS

- Summary of BAT Guidance for New-Build and Retrofit Post-Combustion Carbon Dioxide Capture Using Amine-Based Technologies for Power and CHP Plants Fuelled by Gas and Biomass as an Emerging Technology under the IED for the UK
- <https://www.gov.uk/guidance/post-combustion-carbon-dioxide-capture-best-available-techniques-bat>
- BAT Review for New-Build and Retrofit Post-Combustion Carbon Dioxide Capture Using Amine-Based Technologies for Power and CHP Plants Fuelled by Gas and Biomass as an Emerging Technology under the IED for the UK
- <https://ukccsrc.ac.uk/best-available-techniques-bat-information-for-ccs/>
- IChemE Webinars – BAT for post combustion CCS – John Henderson, EA
 - BAT for ‘Blue’ Hydrogen Production with CCS – Jane Durling, EA
- [ESIG Webinar archive - IChemE](#)

Future BAT Guidance

- BAT guidance for Hydrogen Production by Electrolysis
- Ongoing work to support post-combustion CCS
 - Improved modelling of atmospheric chemistry of amine releases
 - Certified monitoring methods
 - Develop more EALs for amine solvents & degradation products
 - Decarbonisation clusters and multiple sources of amines
- Other BAT guides to support Net Zero delivery
- Other BAT guidance needed?

How does BAT fit with the UK's Hydrogen Strategy?

- Advising as part of the HAC Standards and Regulations WG
- Identify any interactions with current environmental regulations
 - e.g. CO₂ equivalent accounting method
- [UK hydrogen strategy - GOV.UK \(www.gov.uk\)](https://www.gov.uk/government/consultations/uk-hydrogen-strategy)
- [Designing a UK low carbon hydrogen standard - GOV.UK \(www.gov.uk\)](https://www.gov.uk/government/consultations/designing-a-uk-low-carbon-hydrogen-standard)
 - Consultation on standard now closed

Thank you

Any Questions?

Email: jane.durling@environment-agency.gov.uk

Appendices for Reference

Recent US paper on carbon intensity of 'blue' hydrogen production

	Howarth & Jacobson	UK: domestic gas	UK: US LNG	
Leakage rate from production and delivery	3.5%	0.5%	3.5%	
Upstream CH4 emissions	1.11	0.1	1.11	gCH ₄ /MJ H ₂
Global warming potential (GWP)	86	28	28	
Upstream emissions	102	3	31	gCO ₂ e/MJ H ₂
SMR plant efficiency with CCS	56%	79% [*]	79% [*]	MJ H ₂ /MJ CH ₄
CO2 capture rate	62%	95% [*]	95% [*]	
CO2 released from the SMR to the atmosphere	33	3	3	gCO ₂ /MJ H ₂
Total emissions	135	7	34	gCO₂e/MJ H₂
Emissions from the UK residential sector				
Residential natural gas use		58	88	MtCO ₂ e
If blue hydrogen replaced all natural gas		7	36	MtCO ₂ e

* JM LCH™ process

* UK TIMES energy system model

Data on slide courtesy of Paul Dodds, UCL

Equilibrium reactions (BAT review)

Table 15 – Steam Methane Reforming and Shift Chemical Reactions

Chemical Reactions		
Steam Methane Reforming	$\text{CH}_4 + \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO} + 3 \text{H}_2$	$\Delta H_{298} = 206 \text{ kJ/mol}$
Water Gas Shift	$\text{CO} + \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{H}_2 + \text{CO}_2$	$\Delta H_{298} = -41 \text{ kJ/mol}$
Overall Reaction *	$\text{CH}_4 + 2 \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO}_2 + 4 \text{H}_2$	$\Delta H_{298} = 165 \text{ kJ/mol}$

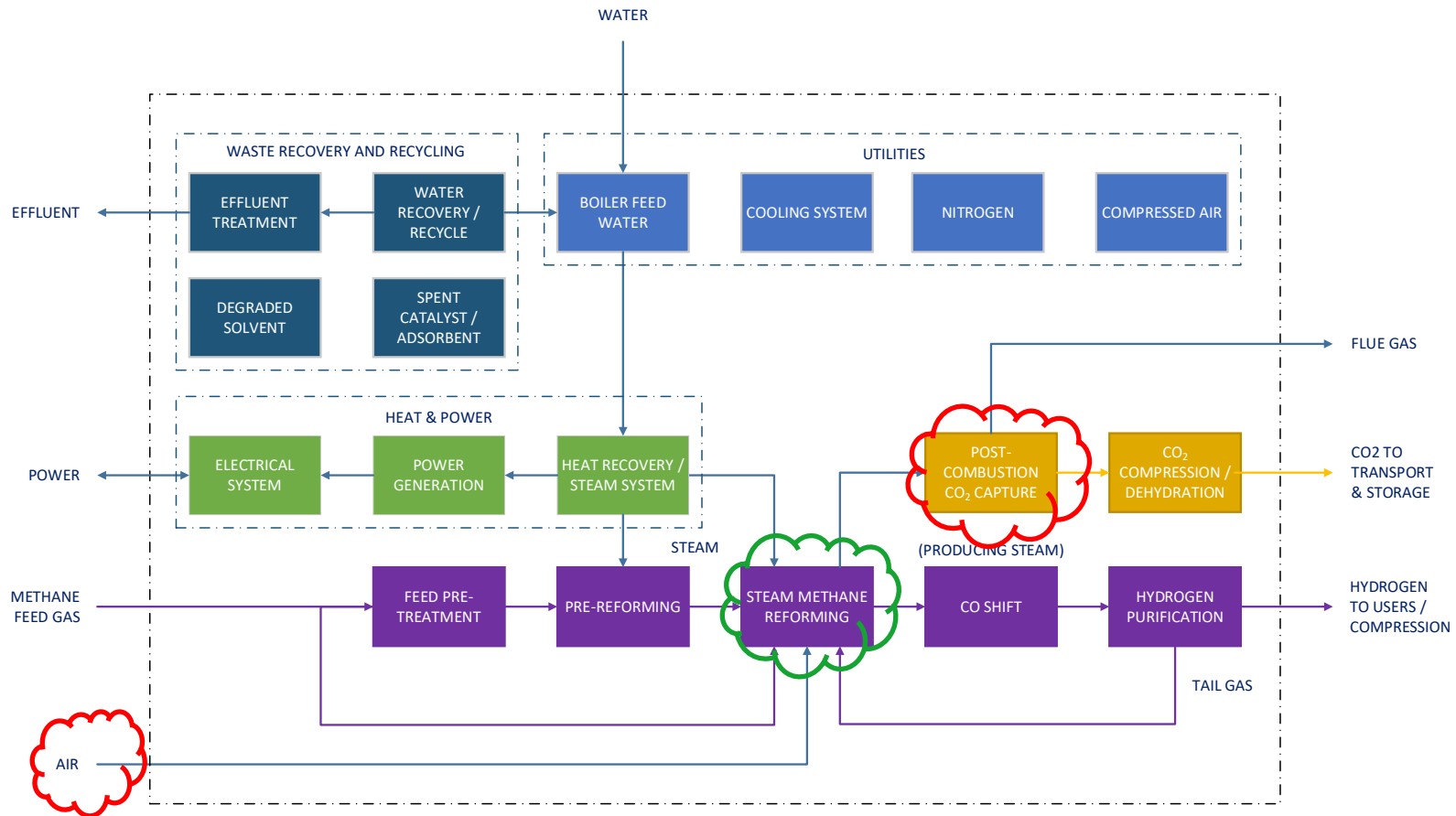
Table 16 – Autothermal Reforming and Shift Chemical Reactions

Chemical Reactions		
Methane Partial Oxidation	$\text{CH}_4 + \frac{1}{2} \text{O}_2 \rightleftharpoons \text{CO} + 2 \text{H}_2$	$\Delta H_{298} = -36 \text{ kJ/mol}$
Steam Methane Reforming	$\text{CH}_4 + \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO} + 3 \text{H}_2$	$\Delta H_{298} = 206 \text{ kJ/mol}$
Combined ATR Reaction *	$\text{CH}_4 + \frac{1}{4} \text{O}_2 + \frac{1}{2} \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO} + \frac{5}{2} \text{H}_2$	$\Delta H_{298} = 85 \text{ kJ/mol}$
Water Gas Shift	$\text{CO} + \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{H}_2 + \text{CO}_2$	$\Delta H_{298} = -41 \text{ kJ/mol}$
Overall Reaction	$\text{CH}_4 + \frac{1}{4} \text{O}_2 + \frac{3}{2} \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO}_2 + \frac{7}{2} \text{H}_2$	$\Delta H_{298} = 44 \text{ kJ/mol}$

Table 17 – Partial Oxidation and Shift Technology Chemical Reactions

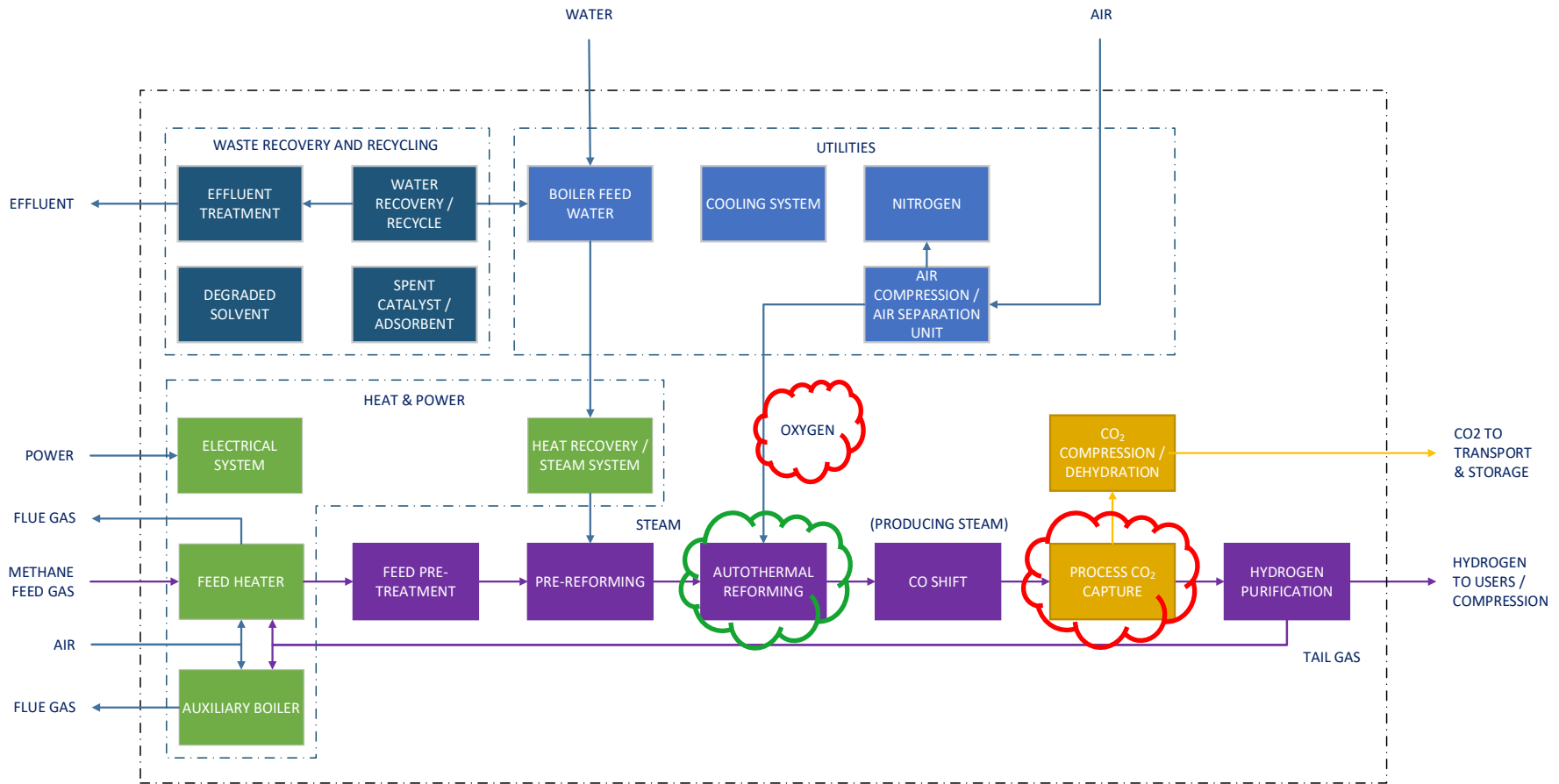
Chemical Reactions		
Methane Partial Oxidation	$\text{CH}_4 + \frac{1}{2} \text{O}_2 \rightleftharpoons \text{CO} + 2 \text{H}_2$	$\Delta H_{298} = -36 \text{ kJ/mol}$
Water Gas Shift	$\text{CO} + \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO}_2 + \text{H}_2$	$\Delta H_{298} = -41 \text{ kJ/mol}$
Overall Reaction	$\text{CH}_4 + \frac{1}{2} \text{O}_2 + \text{H}_2\text{O}_{(\text{g})} \rightleftharpoons \text{CO}_2 + 3 \text{H}_2$	$\Delta H_{298} = -77 \text{ kJ/mol}$

Steam Methane Reforming Process



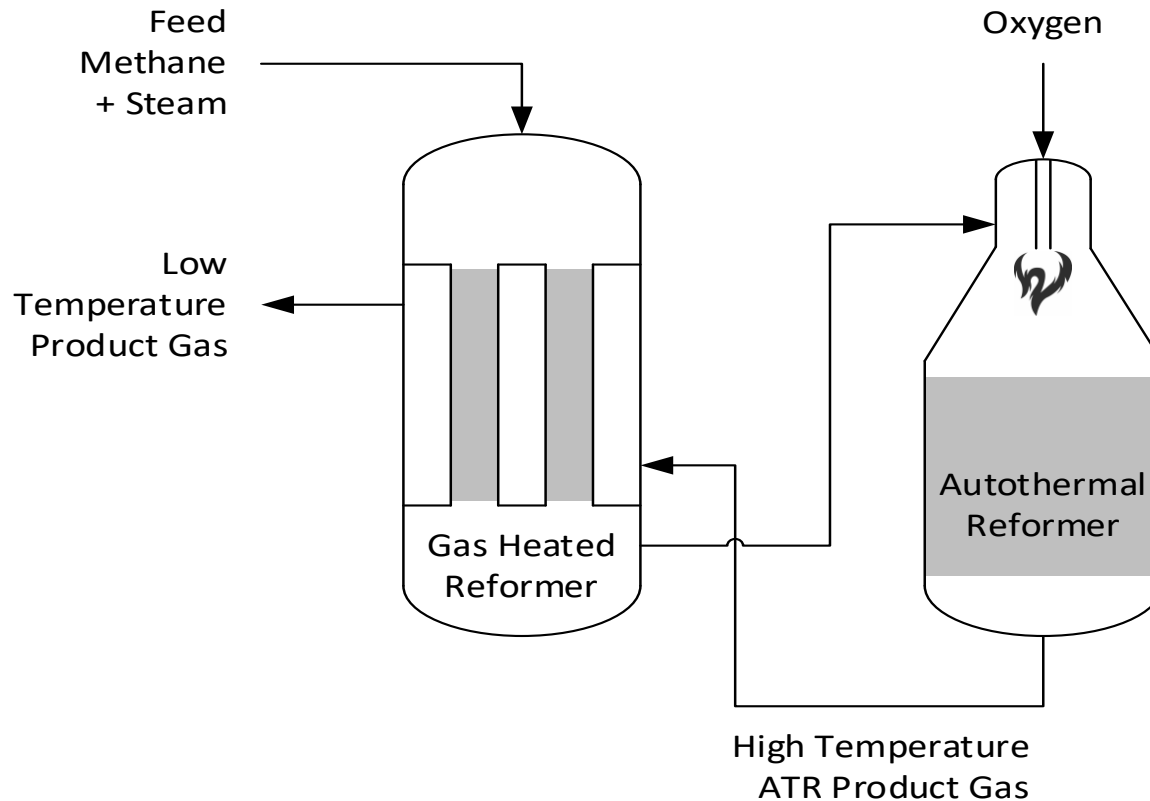
Block Flow Diagram of SMR Technology with Carbon Capture
(Typical – Other Configurations are Possible)

Autothermal Reforming Process

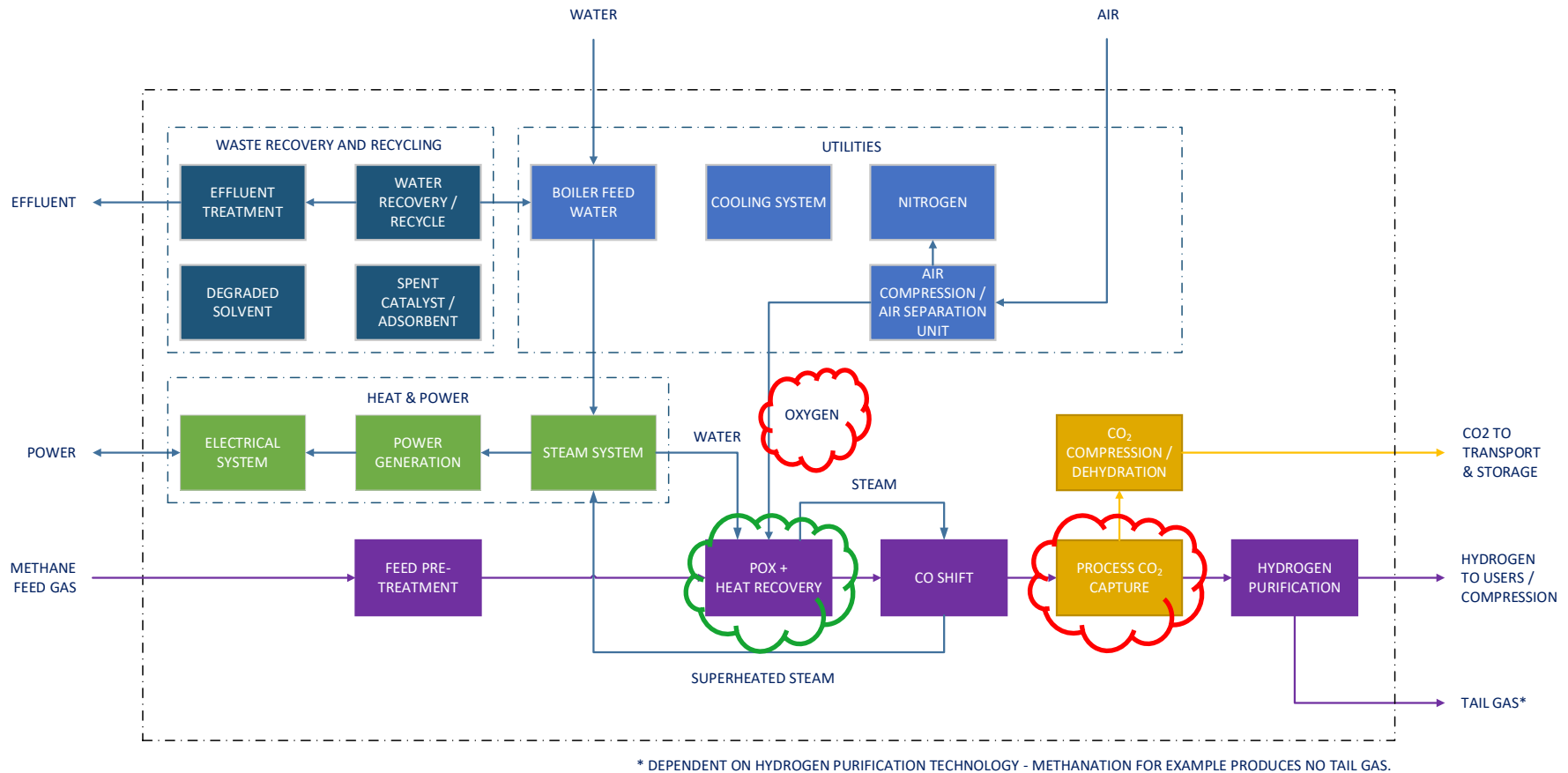


Block Flow Diagram of ATR Technology with Carbon Capture
(Typical – Other Configurations Possible, e.g. with Addition of Gas Heated Reformer)

Gas Heated Reforming Process e.g. GHR+ATR in series



Gas POX (Partial Oxidation) Process



**Block Flow Diagram of POX Technology with Carbon Capture
(Typical – Other Configurations are Possible)**