

1. Introduction

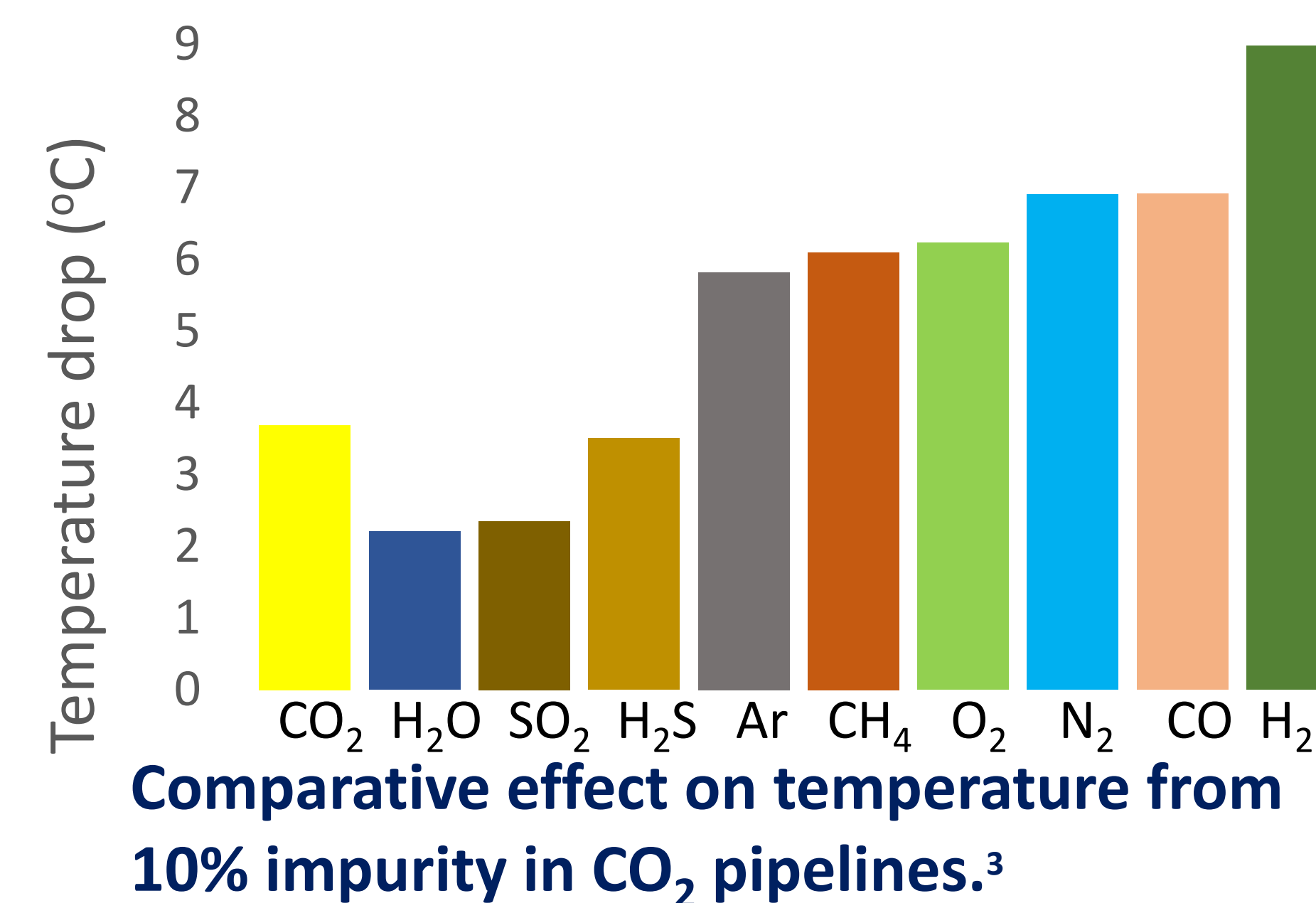
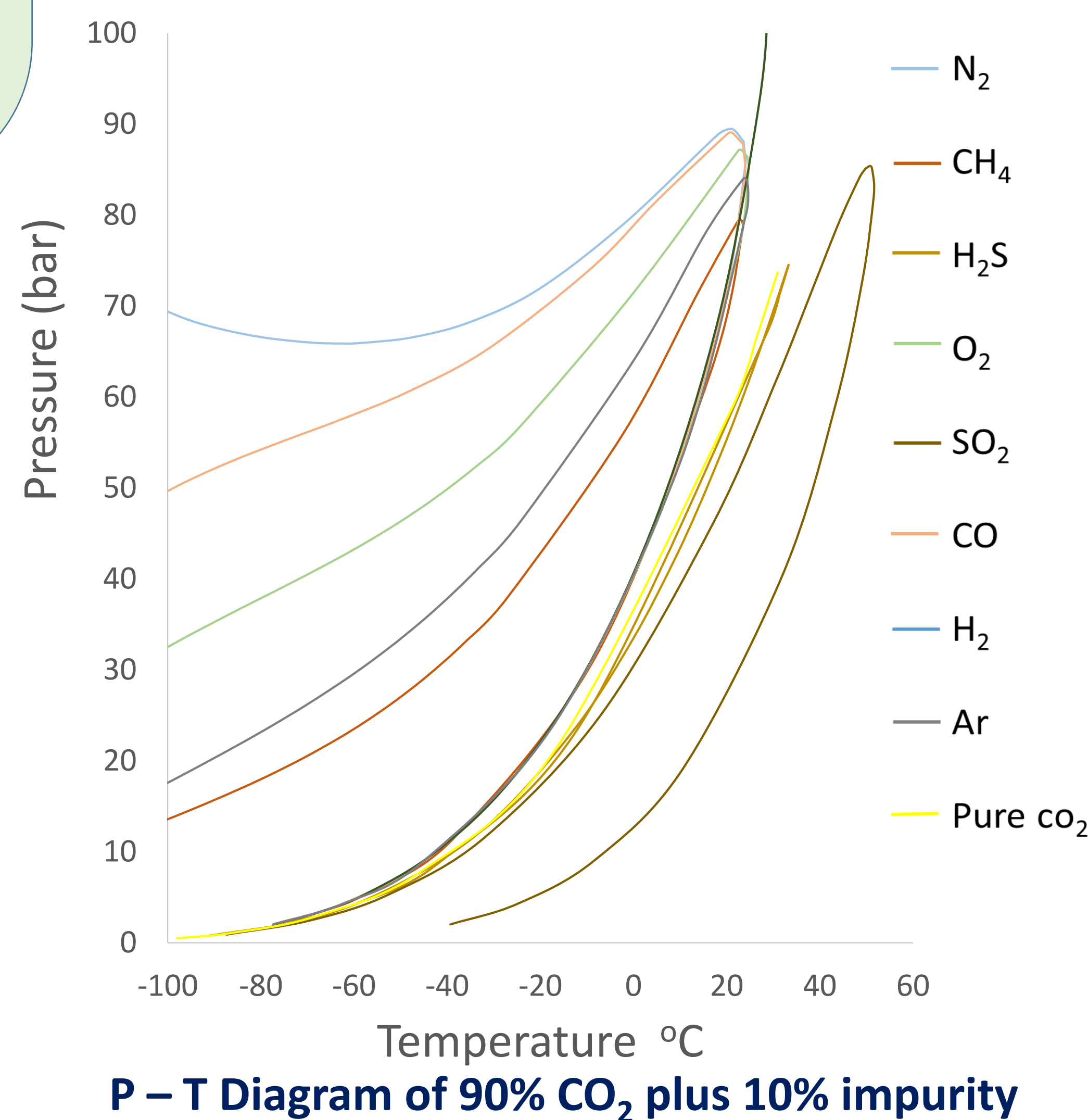
- ❖ CO₂ is captured from large emission sources, transported to storage locations and stored in saline aquifers.
- ❖ Pipelines are used in the onshore and offshore transportation of CO₂ fluids.
- ❖ CO₂ fluids flowing in pipelines contain impurities.^{1,2}
- ❖ Impurities in CO₂ pipelines include: N₂, CH₄, H₂S, SO₂, H₂, O₂, Ar, H₂O, CO, etc.¹
- ❖ Impurities affect flow behaviour of CO₂ fluids in pipelines.
- ❖ Understanding the effect of these impurities will improve the design of CO₂ pipelines.

2. Methodology

- ❖ Aspen HYSYS, gPROMS and HydraFlash are used to simulate
 - Change in pressure,
 - Change in temperature,
 - Critical pressure and temperature,
 - and Hydrate formation conditions.
- ❖ Pseudo fluids of 90% CO₂ and 10% impurity are assumed.
- ❖ Inclined, horizontal and downhill pipelines are considered.

3. Results

- ❖ In the horizontal pipeline, H₂ and SO₂ resulted to the highest and lowest pressure losses, respectively.
- ❖ In the inclined pipeline, SO₂ and H₂ caused the highest and lowest pressure losses, respectively.
- ❖ In the downhill pipeline, SO₂ had the highest pressure gain while H₂ was the only impurity that caused a pressure loss.
- ❖ H₂ and SO₂ respectively caused the highest and lowest temperature losses.
- ❖ H₂ and H₂S created the widest and narrowest 2-phase regions, respectively.
- ❖ Hydrate formation temperature was increased mostly by N₂ and decreased mostly by H₂S.
- ❖ All impurities increased the critical pressure. The highest and lowest increases are from H₂ and H₂S respectively.
- ❖ Only H₂S and SO₂ increased the critical temperature. The lowest critical temperature is with CH₄.

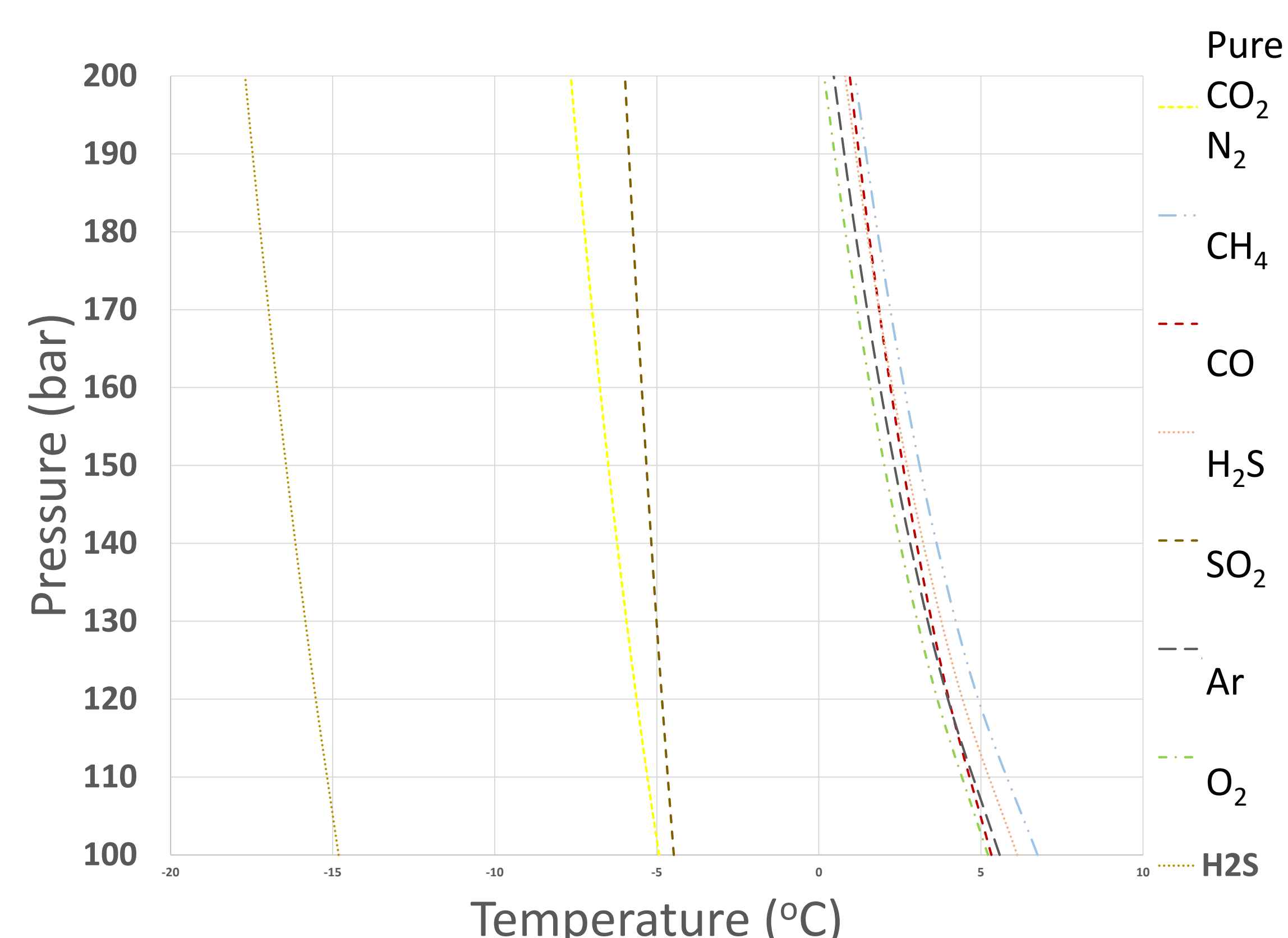
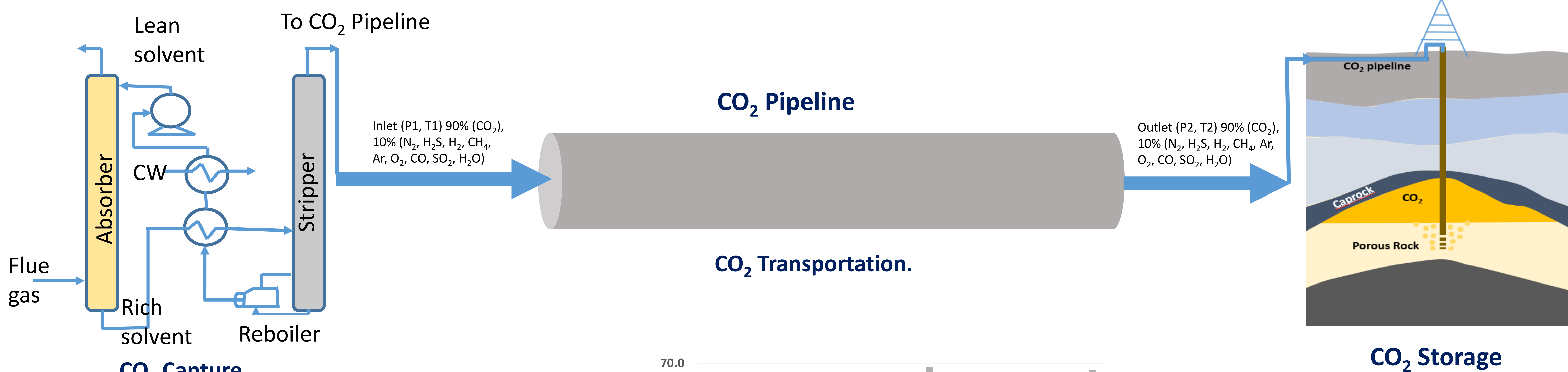


Bubble and Dew points of 90% CO₂ and 10% impurity at 0 °C

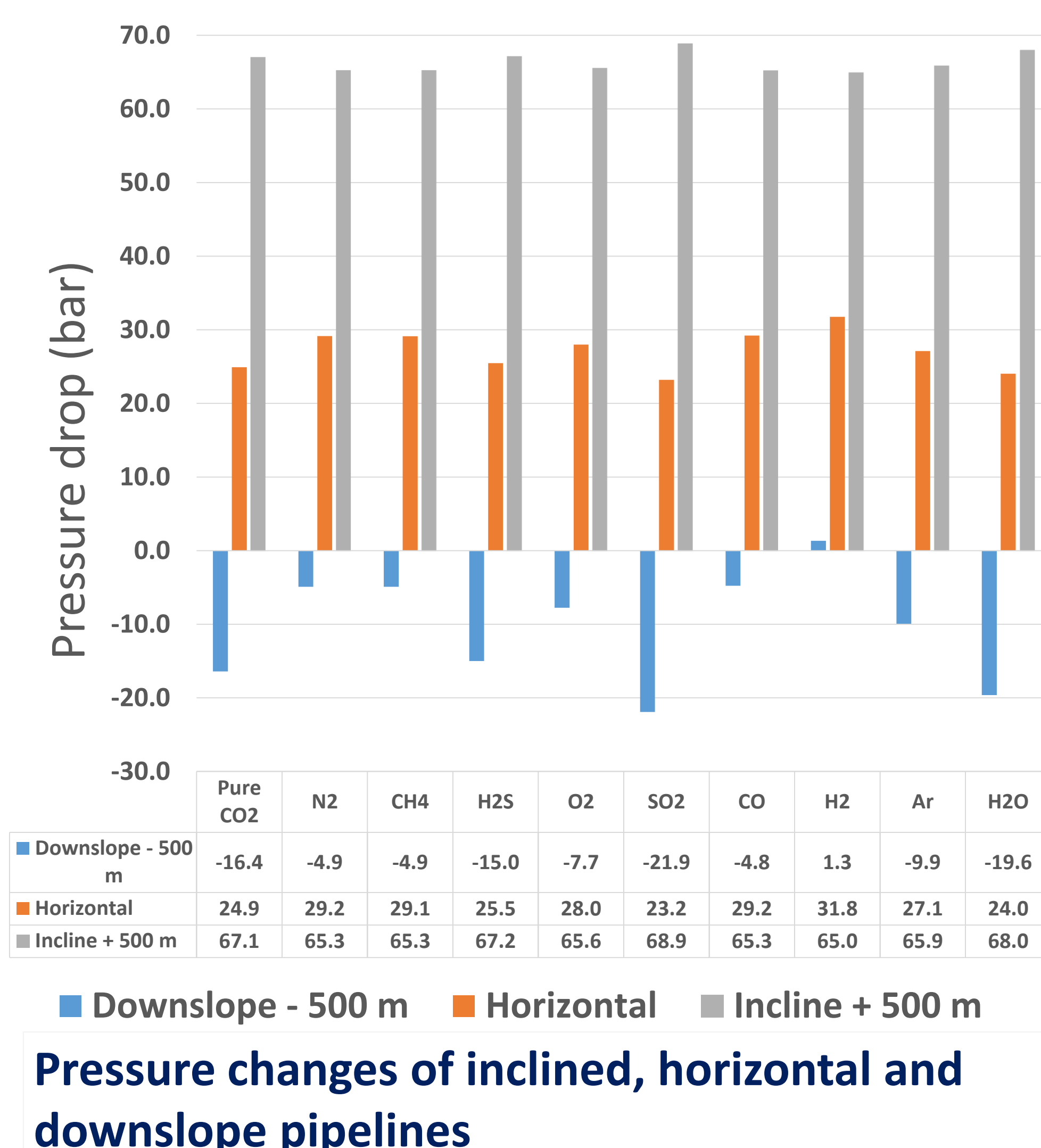
Components	P _b (bar)	P _d (bar)	ΔP _d
CO ₂ + N ₂	80	40	40
CO ₂ + CH ₄	58	40	18
CO ₂ + H ₂ S	34.8	33.4	1.4
CO ₂ + SO ₂	30.5	12.7	17.8
CO ₂ + CO	79	41	38
CO ₂ + O ₂	72	40	32
CO ₂ + H ₂	140	40	100
CO ₂ + Ar	64	40	24

Critical pressure and critical temperature of 90% CO₂ and 10% impurity.³

Components	Pure CO ₂	CH ₄	N ₂	H ₂ S	O ₂	SO ₂	CO	NO	Ar	H ₂
P _c (bar)	73.7	79.39	88.15	74.53	86.44	85.11	87.83	89.10	83.73	107.7
T _c (°C)	30.95	23.25	23.61	33.29	24.41	49.84	23.48	24.83	24.39	28.34



Hydrate formation temperatures of 90% CO₂ and 10% impurity between 100 and 200 bar



4. Conclusions

- ❖ Hydrogen has the greatest adverse effect on CO₂ pipelines.
 - ❖ Effects of impurities on pressure also depend on pipeline profile.
 - ❖ Gases with higher densities than CO₂ reduce pressure losses in horizontal pipelines but increase pressure losses in uphill pipelines.
 - ❖ A low critical pressure is desirable because less energy is required to compress gas to supercritical state.
 - ❖ All impurities increase critical pressures, increasing the energy penalty to compress gas.
 - ❖ Only gases containing sulphur increase the critical temperature.
- All impurities introduce errors in the process design of CO₂ pipelines.