

International Forum on Recent Developments of CCS Implementation

Leading the way to a low-carbon future



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CONFIRMED
SPEAKERS &
CALL FOR
ABSTRACTS



26th —27th
MARCH 2015

VENUE

Athens Ledra Hotel, 115 Syngrou Avenue, Athens, Greece

REGISTRATION DEADLINE

Early bird registration (only € 440 including accommodation) is available until the

31st January 2015.

CALL FOR ABSTRACTS

We invite you to submit an abstract for either oral or poster presentation .

Deadline for submissions is the 15th December 2015.

Co-organised by

CO₂QUEST

IoLiCAP

ECR funding is available from



To register <http://goo.gl/xkMVcq>
contact Abigail Ward—a.ward@leeds.ac.uk
or visit www.co2quest.eu

Confirmed Speakers

The organising committee are delighted to announce the following keynote speakers:



Dr. Vassilios Kougionas - DG Research & Innovation, European Commission - "Future EC Funding Strategy and Opportunities in CCS"

Mr. John Gale- General Manager, IEA Greenhouse Gas R&D Programme - "A Global Overview of CCS Implementation"



Dr. Paul Fennel - Reader in Clean Energy, Imperial College London - "Comparative Costings for 1st, 2nd and 3rd Generation CCS technologies "

Mr. Russell Cooper - Technical Services Manager, National Grid, UK - "The White Rose CCS Project"



Call for Abstracts

Abstracts called for the following sessions:

- Whole-systems CCS
- BECCS and Carbon Neutral Technologies
- CCS for CO₂-intensive Industries
- Demonstration Projects
- CO₂ Capture
- CO₂ Storage
- CO₂ Transport
- Materials for CCS
- Governance of Development and Deployment of CCS

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Numerical modelling of trans-triple point temperature near-field sonic dispersion of CO₂ from high pressure dense phase pipelines

Dr Chris Wareing

UKCCSRC Equation of State Workshop,
11th November 2014, York

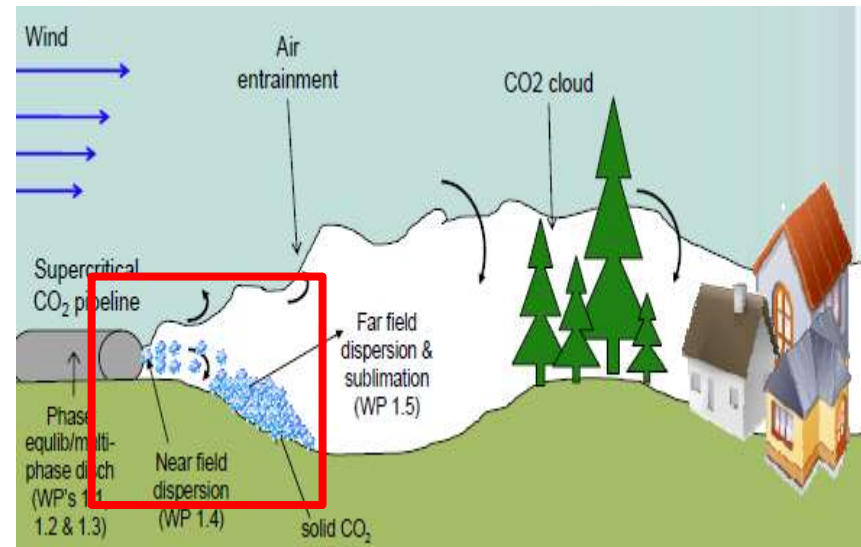
C J Wareing, R M Woolley, M Fairweather, S Falle
University of Leeds, Leeds, LS2 9JT, United Kingdom



COOLTRANS: The Don Valley CCS Project is co-financed by the European Union's European Energy Programme for Recovery
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Carbon capture and storage, the short term option for reducing CO₂ emissions, is likely to proceed with transportation from source to storage along high-pressure dense phase pipelines

- Pipelines fail. Complex CFD simulations can validate pragmatic approaches used for quantified risk assessment (QRA).
- Leeds: near-field sonic dispersion of carbon dioxide (CO₂) from high pressure pipelines
 - Examples
 - Thermodynamic model
 - Recent developments
- Requirements for impurities



Venting: COOLTRANS dense phase

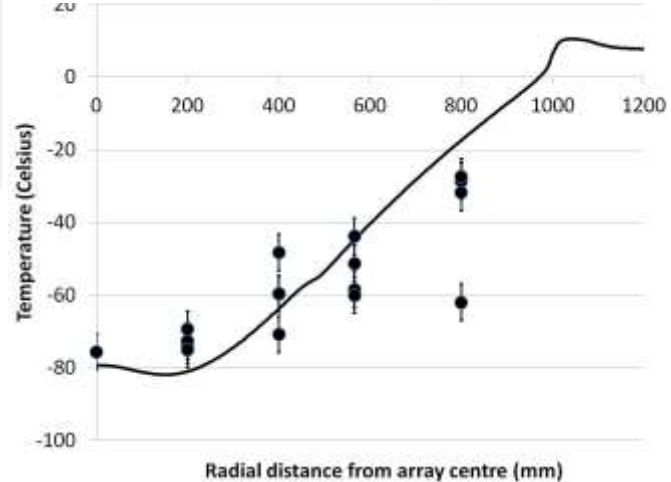
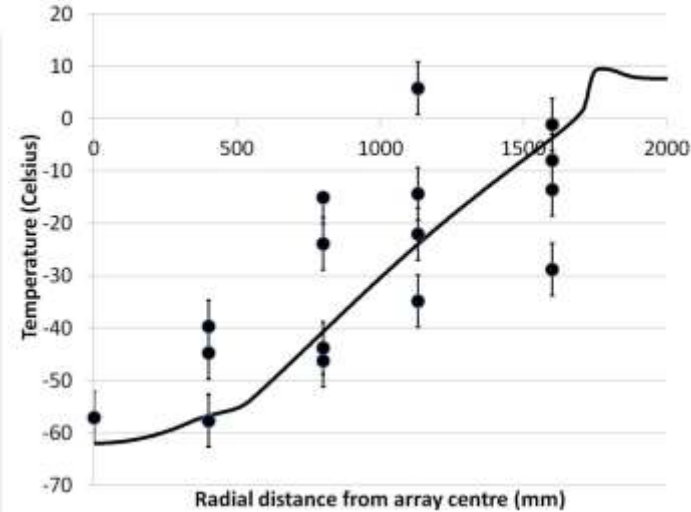
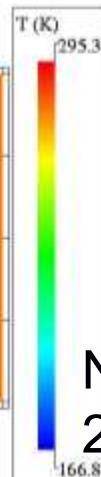
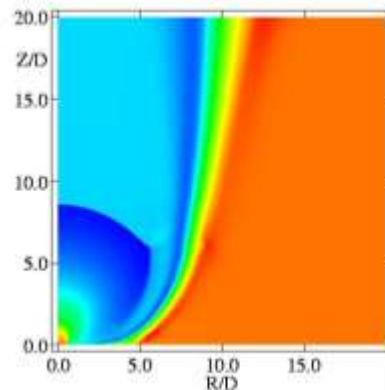
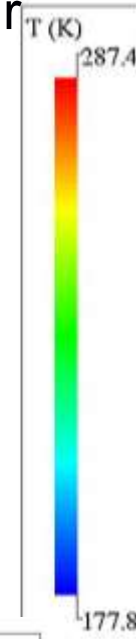
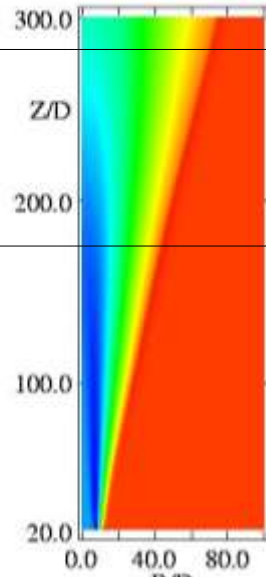


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Dense phase release from a 150bar reservoir through a 25mm ventpipe

Measurements at:

- 4m (165D)
- 7m (288D)



Near-field shock containing region:
20D x 20D (0.5m x 0.5m)

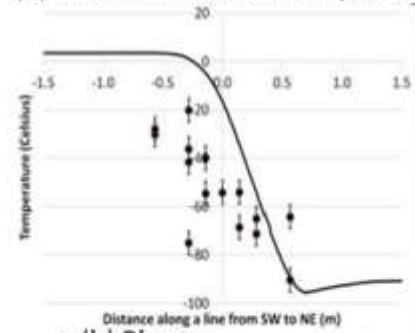
COOLTRANS punctures and ruptures



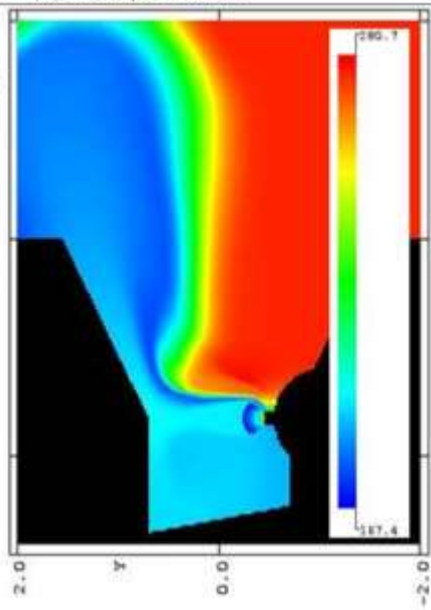
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Puncture:

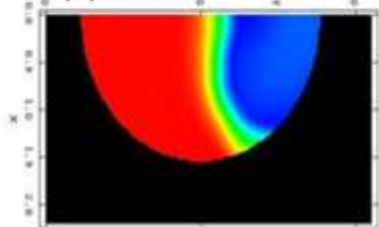
(a) Data vs. model on 1m plane



(c) Side puncture

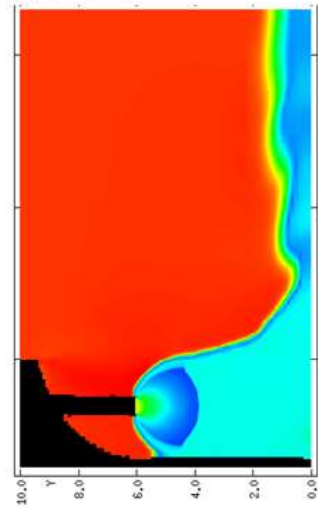


(b) Plane

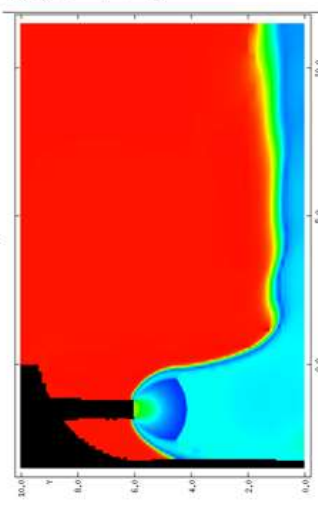


Rupture:

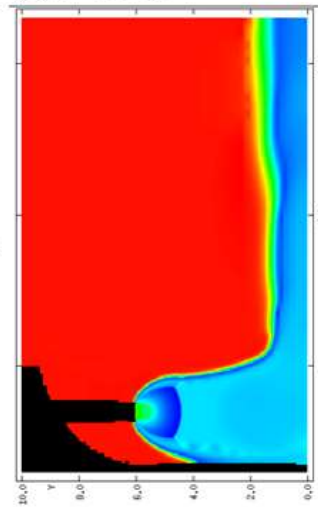
(a) t=30s



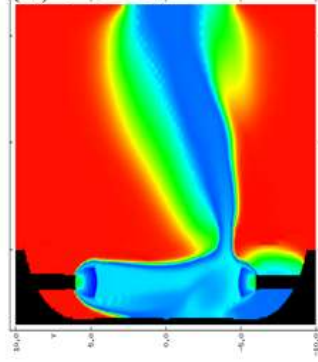
(b) t=100s



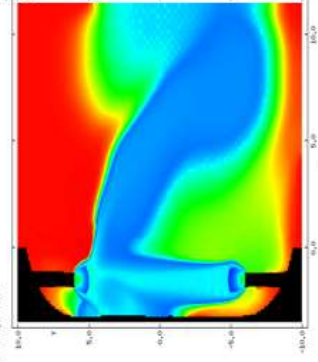
(c) t=250s



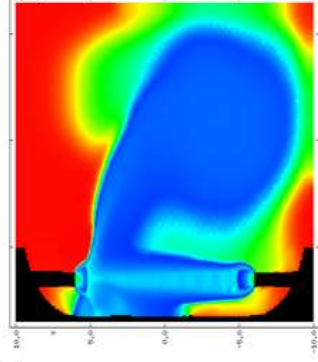
(d) t=600s



(e) t=1000s



(f) t=1150s



-100°C

Temperature



Near-field dispersion model (COOLTRANS & CO2PIPEHAZ)



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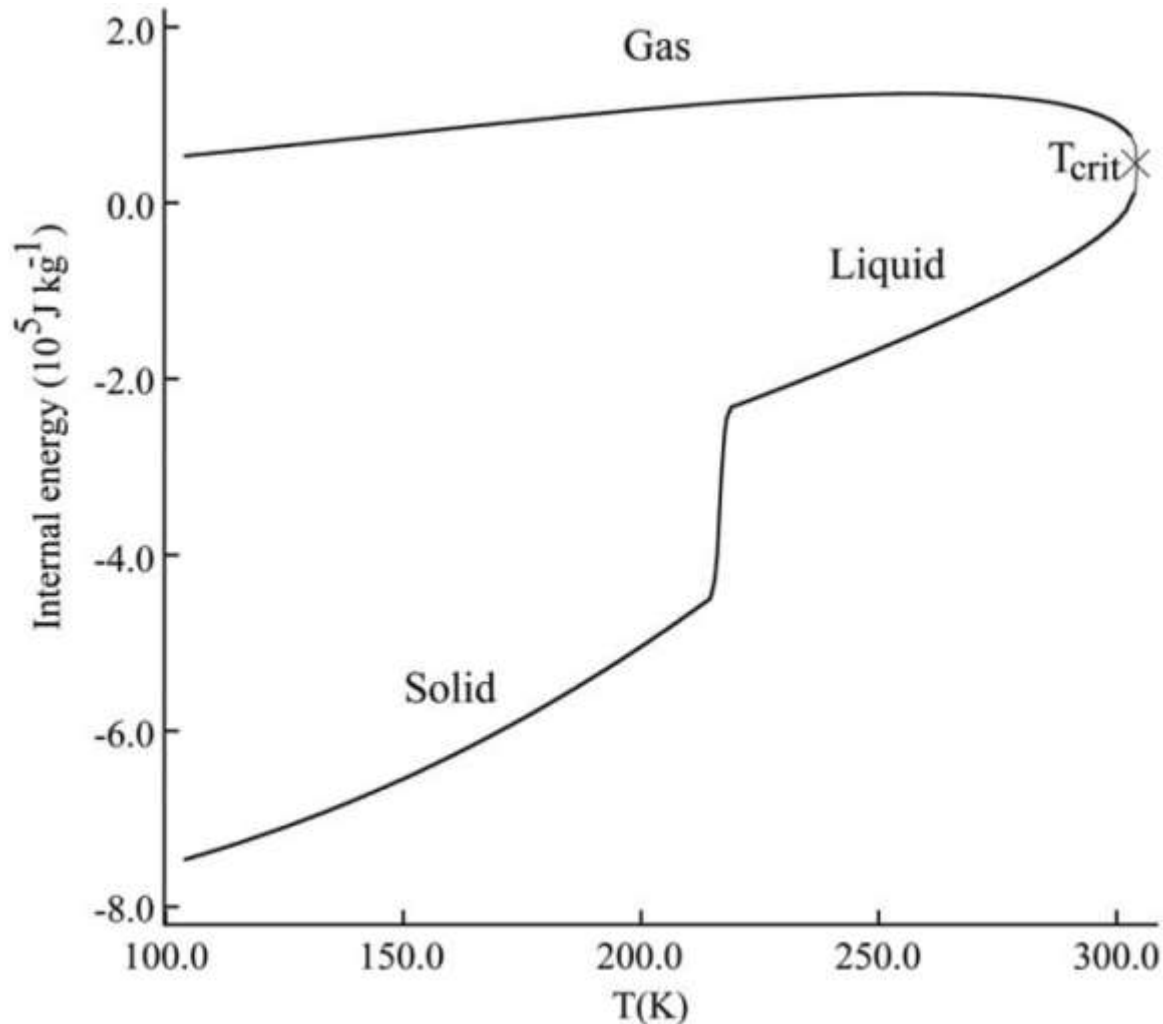
- Thermodynamic model: *(Wareing et al. 2013, AIChE Journal 59 3928-3942)*
- Near-field dispersion of pure CO₂ in the gas, liquid and solid phases into dry air.
- Novel composite equation of state for pure CO₂ employing:-
 - the **Peng-Robinson** equation of state in the gas phase;
 - tabulated data derived from the **Span & Wagner** equation of state for the liquid phase and vapour pressure;
 - and **NIST/DIPPR data** for the solid phase and latent heat of fusion.
- Calculations were undertaken using the **Helmholtz free energy** in terms of temperature and molar volume, as all other thermodynamic properties can be readily obtained from it.
- Novel combination of the simple Peng-Robinson equation and tabulated data on the saturation line allows for crucially a **fast implementation numerically**, when updating **tens of millions of grid cells per second**.

Near-field dispersion model (COOLTRANS & CO2PIPEHAZ)

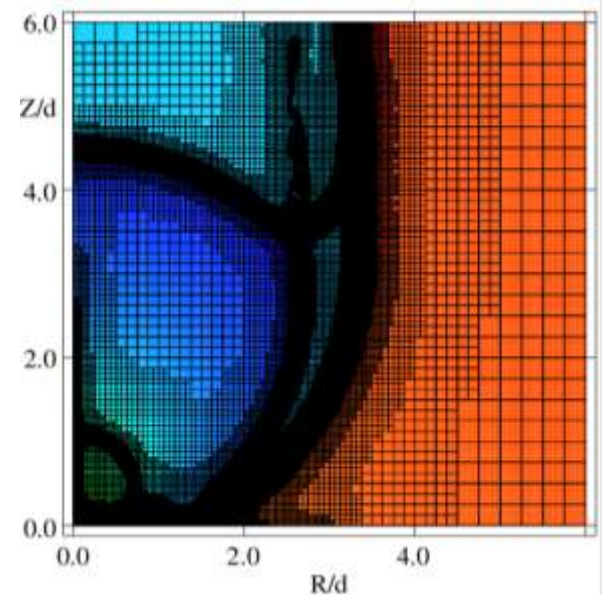


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- Internal energy on the saturation line.



- T_{crit} marks the critical temperature.
- The triple point can be identified by the steep connection between the liquid and solid phases – the latent heat of fusion.
- Numerical method, with unstructured AMR



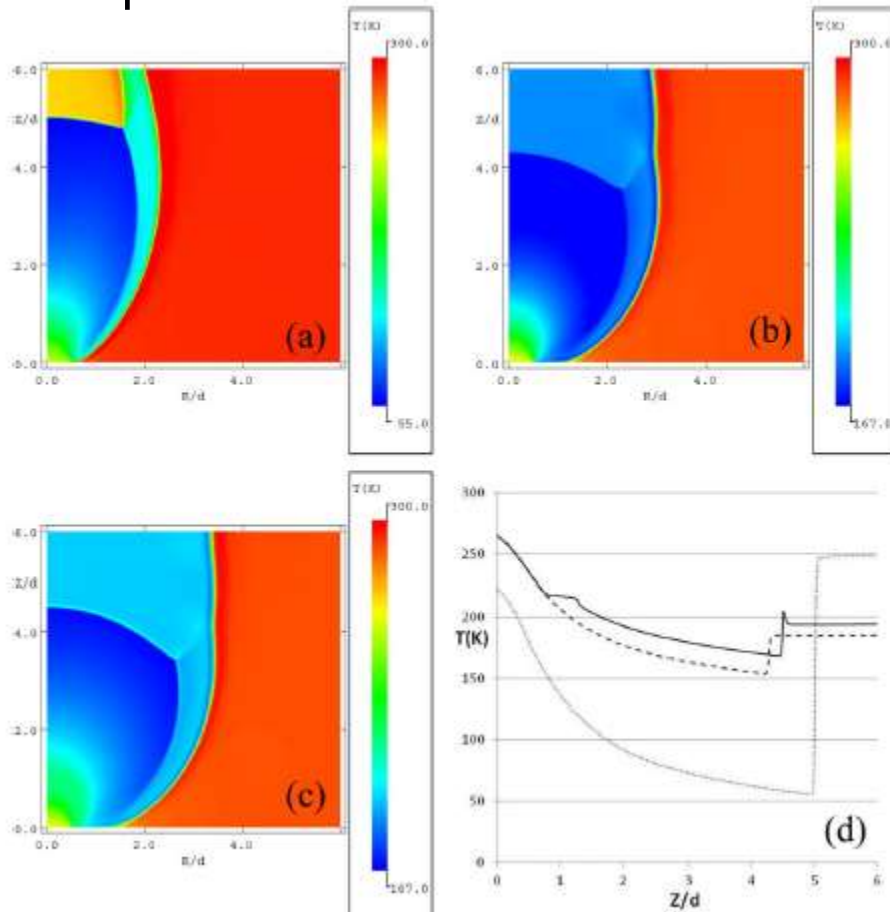
Comparative performance



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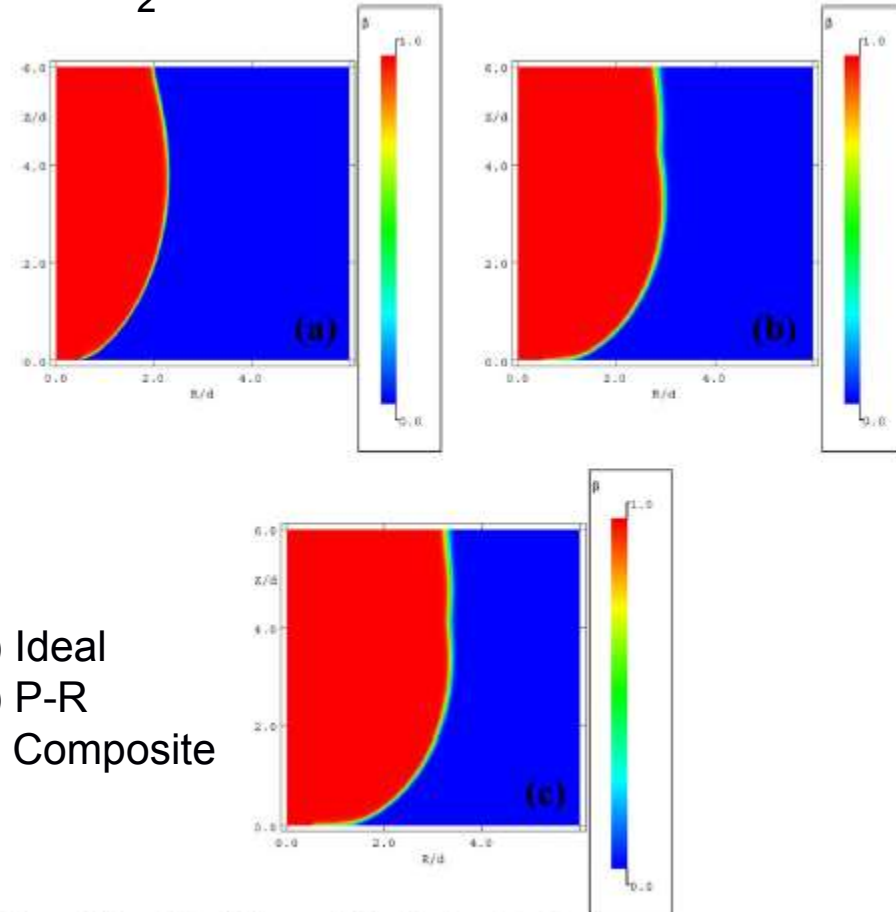
- Comparison of ideal, Peng-Robinson and composite EoSs

Temperature:-



Temperature in the near-field of the flow domain.

CO₂ fraction:-



Concentration of CO₂ in the near-field of the flow domain.

- (a) Ideal
- (b) P-R
- (c) Composite

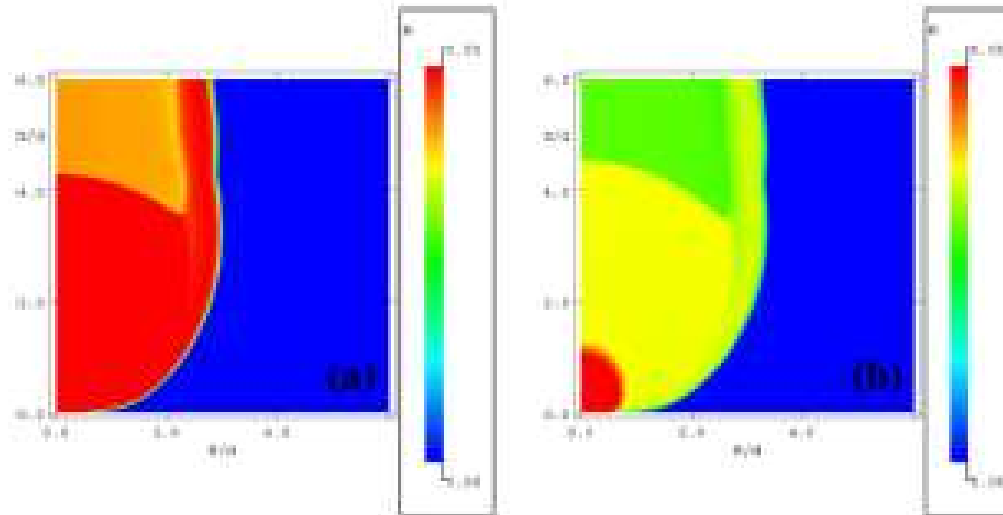
Comparative performance



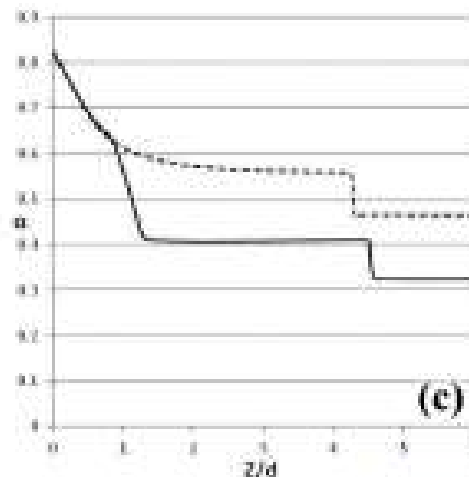
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- Comparison of Peng-Robinson and composite EoSs

Condensed phase fraction:



(a) P-R
(b) Composite



Concentration of condensed-phase CO_2 in the near-field of the flow domain.



- Different equations of state
 - Solid phase. Now able to run with tables generated from Jager and Span – C_p and internal energy are very different. Also considered the Trusler solid phase EoS.
 - Gas and liquid phases. Several equations of state under consideration and comparison:-
 - Physical Properties Library (SAFT/pcSAFT) from the National Research Centre for Physical Sciences, Greece.
 - Tables based on Span and Wagner
 - Tables based on Richard Graham's work.
 - New considerations of EOS-CG.
- Have previously considered PRSV, PRSV2, Yokozeki, PROPATH & others and discounted them for our use.

Requirements for impurities (CO2QUEST)



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- EITHER a simple fast equation of state that can be directly embedded (advantages of speed and solutions over a wide range).
- OR a complex equation that can generate tables (disadvantage – solvers routinely require solutions outside the tabular ranges).
- Mixing rules with known interaction parameters for e.g. N₂, O₂, Ar, H₂S.
- Pipeline spec.: 96% CO₂, 4% impurities (<2% N₂, <2% O₂ + trace).

Temperature range: 50K – 400K. Pressure range: 0.01 to ~20 MPa.

- Options:-
 - A simple option: e.g. Peng-Robinson. But, there are known issues (incorrect densities, speed of sound, etc. noted again at GHGT12)
 - Trust a library function e.g. PPL. Current issues under investigation.
 - More complex option: EOS-CG in tabular form. Possible issues with H₂O (presented at GHGT12)?

Thank you for listening. Discussion?