

UKCCSRC Gas CCS Meeting  
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**PHASE 1 PROJECT:  
METHANE OXYCOMBUSTION IN A PRESSURISED  
SWIRL STABILISED A GAS TURBINE BURNER.**

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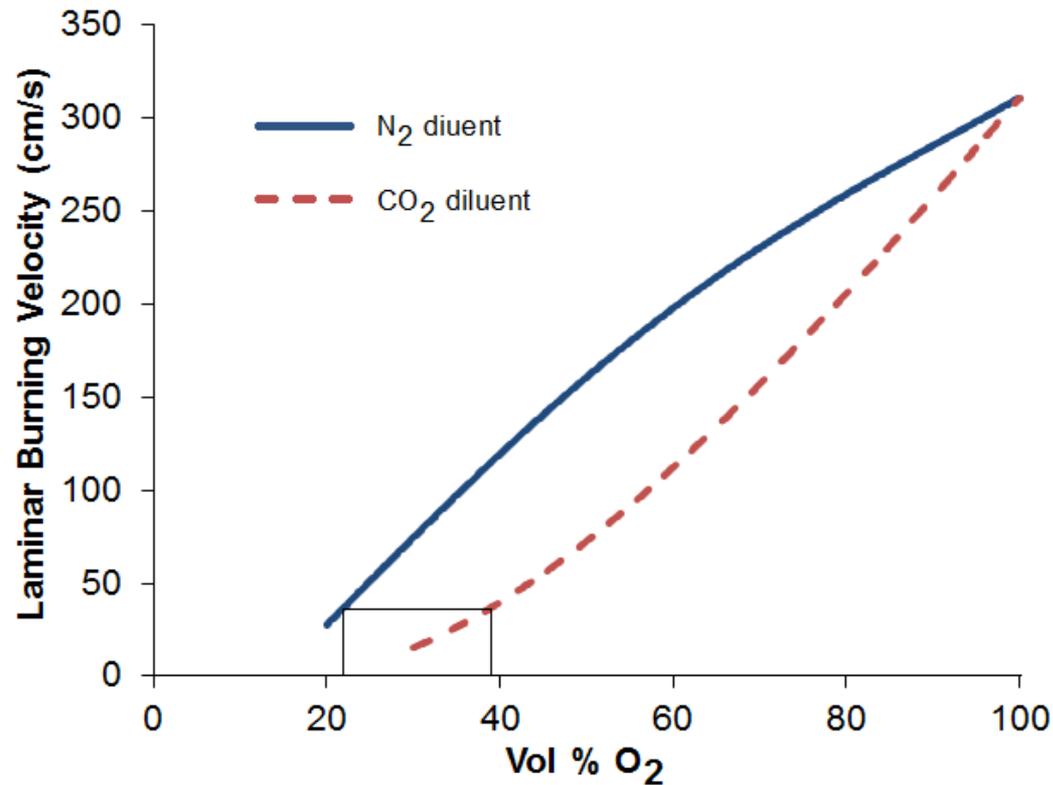
Cardiff University – School of Engineering



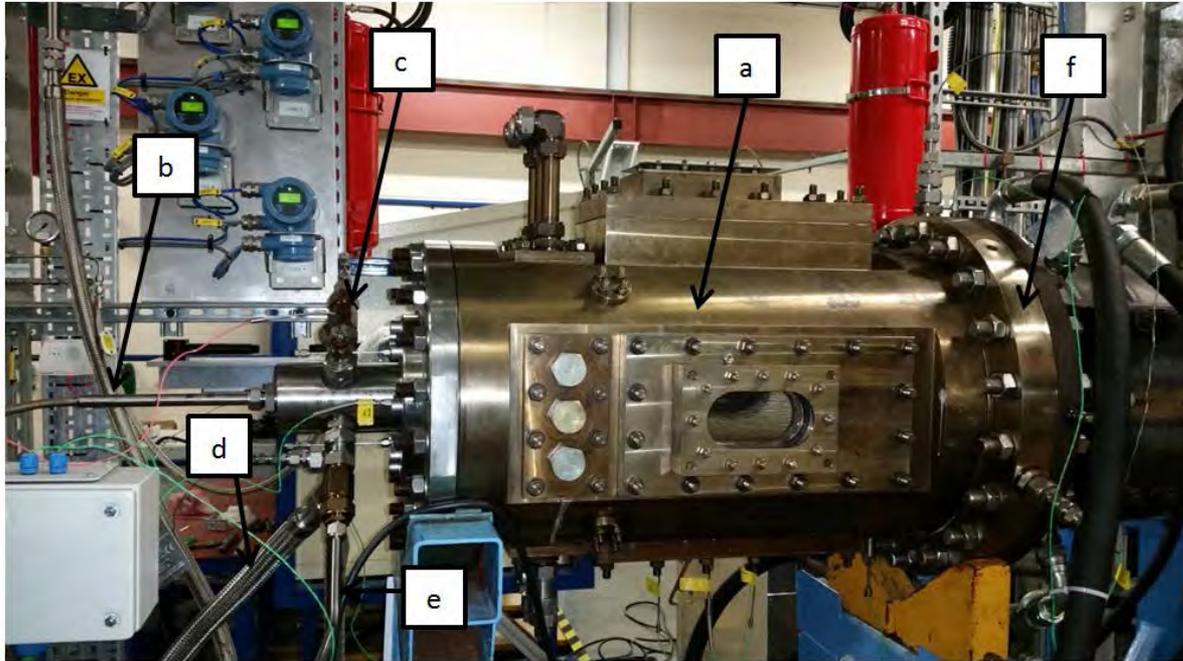
# METHANE OXYCOMBUSTION IN SWIRL STABILISED A GAS TURBINE BURNER.

- A series of combustion experiments at high pressure yielded very interesting and useful data in demonstrating how oxygen and carbon dioxide affect the flame in a gas turbine swirl burner.
- The large swirl burner has been operated at a number of power and pressure settings, up to 50kW and 3 bar pressure. Ran at oxygen concentrations of almost 60% in some cases.
- Added CO<sub>2</sub> to the flame to study the operational effect of simulated exhaust gas recirculation.
- Made gas analysis and chemiluminescence measurements to quantify what is happening in the flame in terms of heat release, location and products of combustion.

# Reminder of oxy / diluent effects



# HPOC with burner and oxygen line

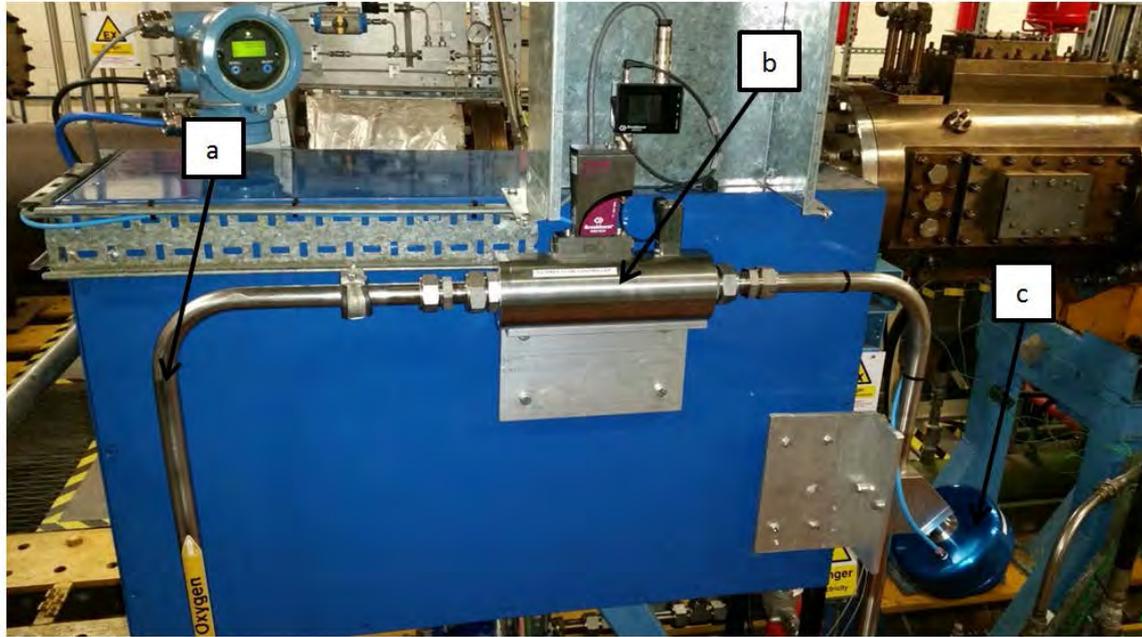


(a) pressure casing (b) spark ignitor (c) fuel line  
(d) air line, (e) oxygen line, (f) exhaust section.

# Burner located in quartz chamber



# Oxygen control system

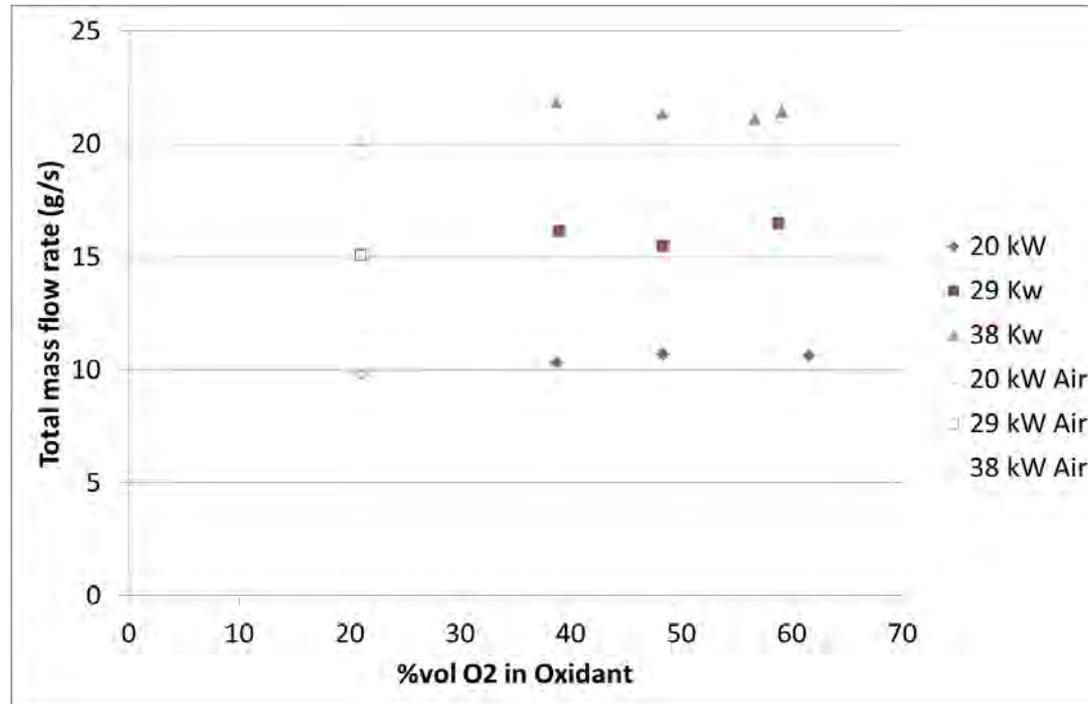


- (a) inflow from reservoir
- (b) mass flow controller and display
- (c) pneumatic cut-off valve.

# Aims

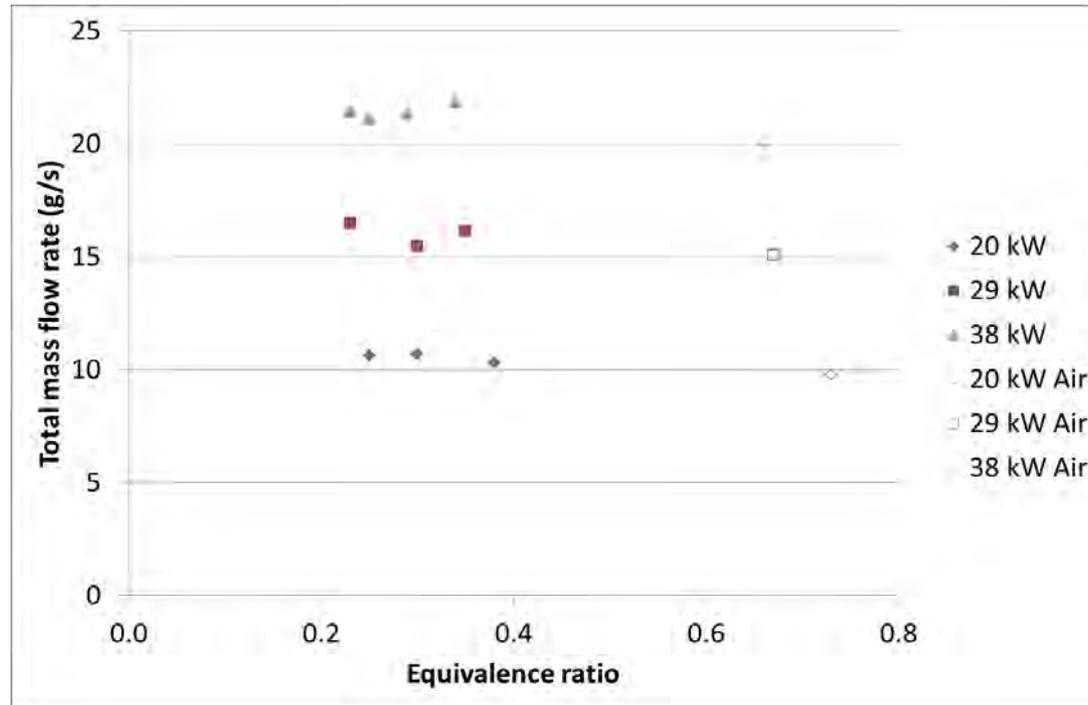
- Testing at small scale atmospheric conditions allowed for the quantification of the stable operating points in a generic burner at variable oxygen and diluent concentrations.
- The larger scale pressurised tests were focussed on showing a smaller number of operating points, to demonstrate the changes in flame shape and emissions.
- Studying  $O_2$  and  $CO_2$  concentrations

# Results – Effect of O<sub>2</sub> concentration



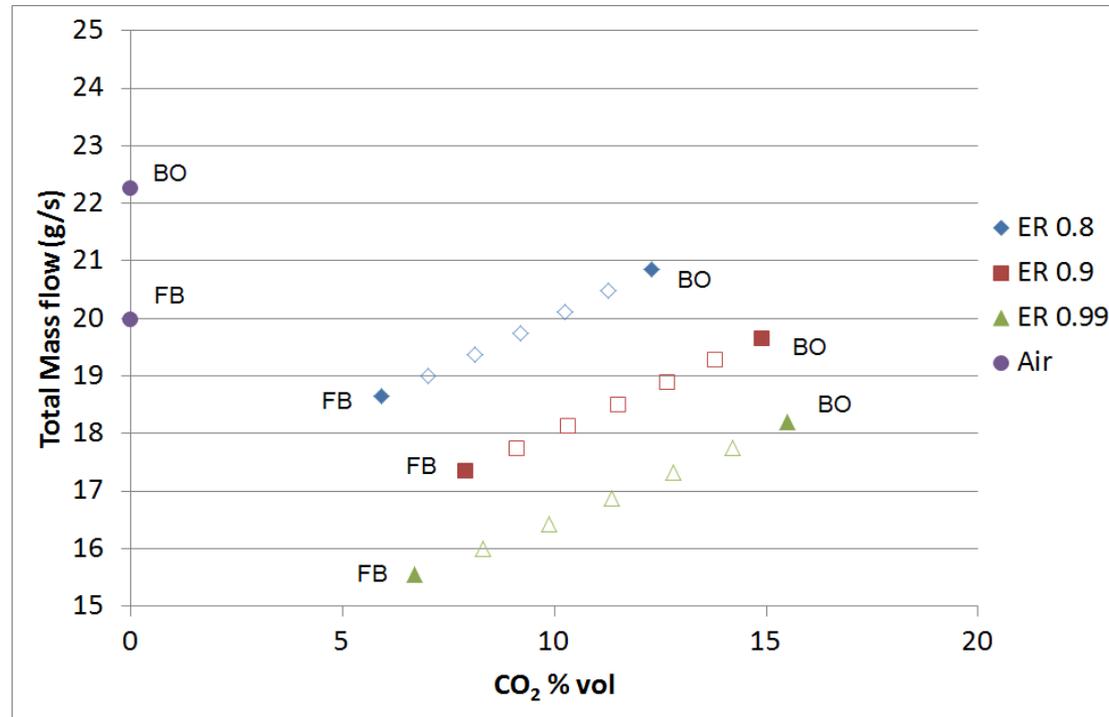
Rich operability limit expressed as total mass flow versus oxygen in oxidant at the 3 power levels examined, plus the equivalent air conditions.

# Results – effect of equivalence ratio



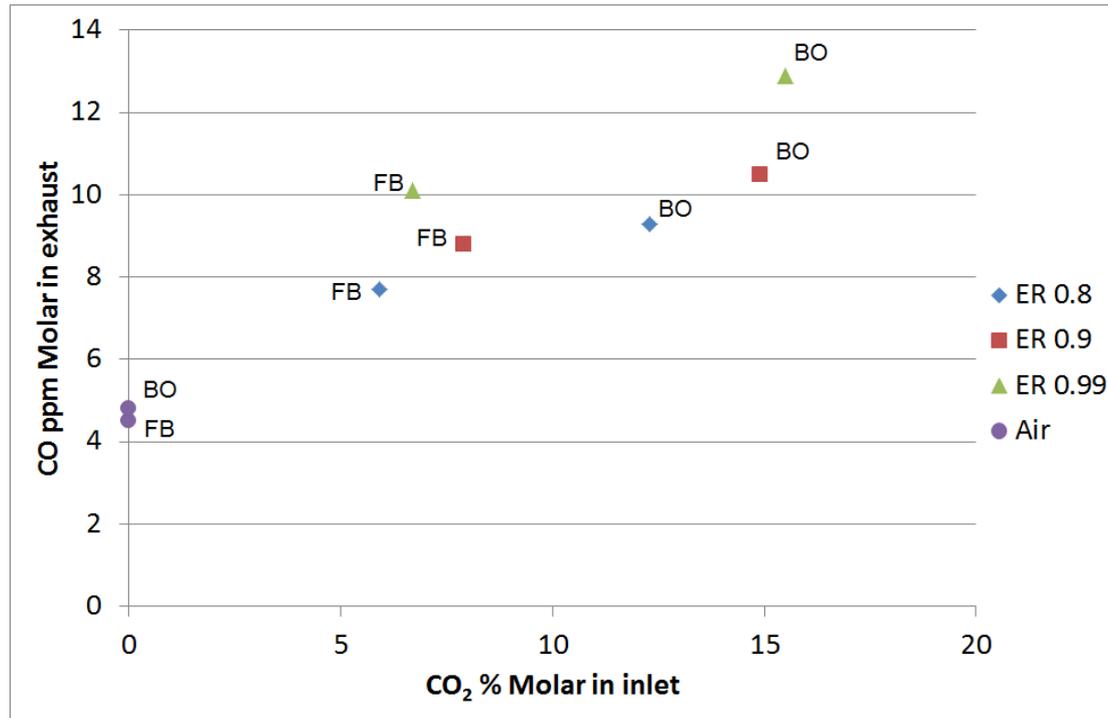
Rich operability limit expressed as total mass flow versus equivalence ratio at the 3 power levels examined showing the **oxygen enhanced conditions**, plus the equivalent air conditions.

# Results – CO<sub>2</sub> diluted tests at 38 kW



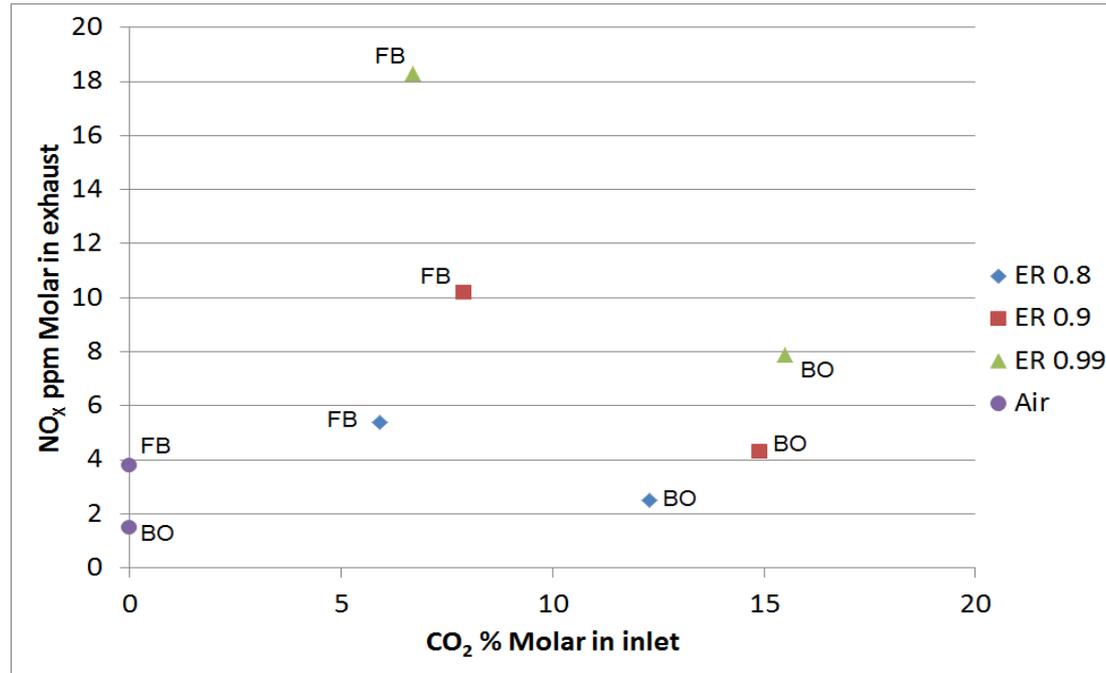
Operation points and limits expressed as total mass flow versus inlet CO<sub>2</sub> concentration at the 3 equivalence ratios, plus the equivalent air conditions.

# Results – CO production during CO<sub>2</sub> diluted operation at 38 kW



Carbon monoxide exhaust concentrations (dry) versus inlet CO<sub>2</sub> concentration at the 3 equivalence ratios, plus equivalent air conditions.

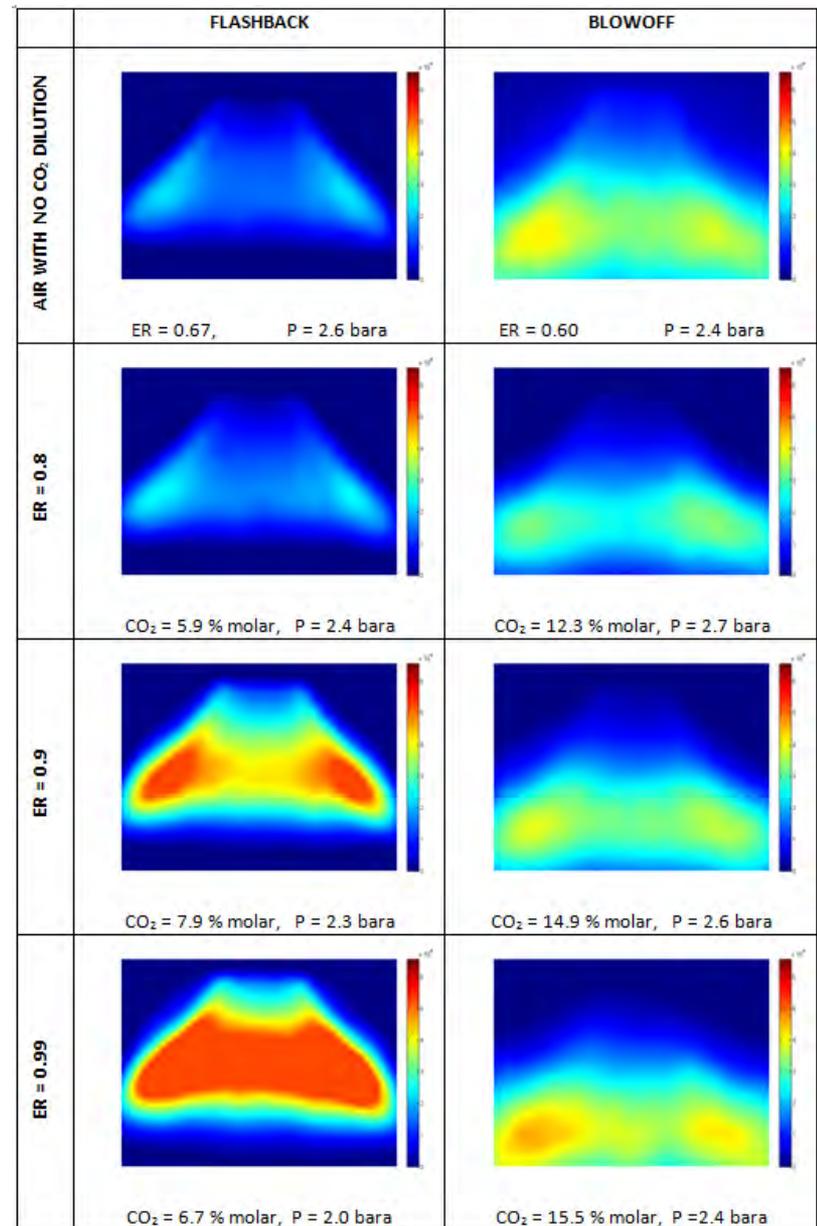
# Results - NO<sub>x</sub> production during CO<sub>2</sub> diluted operation at 38 kW



NO<sub>x</sub> exhaust concentrations (dry) versus inlet CO<sub>2</sub> concentration at the 3 equivalence ratios, plus the equivalent air conditions.

Single false colour chemiluminescence images of 37.5 kW flame at 3 equivalence ratios with varying CO<sub>2</sub> levels to provide flashback and blowoff conditions.

When the CO<sub>2</sub> concentration is increased, with reducing air towards the stoichiometric condition, it can be seen that the OH\* emission becomes more concentrated over the flame zone, which is consistent with the observed increase in NO<sub>x</sub> shown in previous slide



- The presence of high concentrations of oxygen does not significantly affect the operational envelope of the burner in terms of mass flow rate. This is explained by the dilution effect of the excess  $O_2$ , effectively replacing the role of  $N_2$  in the flame as a diluent and combustion moderator. Since  $O_2$  and  $N_2$  have very similar physical properties, the flame appears unchanged.
- It has been possible to operate the swirl burner with high  $O_2$  concentrations at elevated pressure. This is not favourable in terms of the operation of a carbon capture plant, thus EGR to enhance  $CO_2$  concentrations is an important consideration.
- Testing to simulate potential operation of a pressurised swirl burner with EGR has been successful.
- The presence of  $CO_2$  in the reactants causes a reduction in the burning velocity of the mixture and acts as a greater heat sink than atmospheric  $N_2$ . Subsequently stable operation at elevated pressure was achieved at lower mass flows than air operation.

- It was possible to run the burner at stoichiometric levels of air and methane when CO<sub>2</sub> was used as a diluent. This meant that the dry exhaust gas concentration comprised mostly of CO<sub>2</sub> and N<sub>2</sub> only.
- The highest molar CO<sub>2</sub> inlet concentration achieved during this test was 15.5%, which provided a (dry) molar exhaust gas CO<sub>2</sub> concentration of 29%, with the remainder N<sub>2</sub>.
- There is strong evidence to suggest that (diluent) CO<sub>2</sub> will dissociate in the flame, leading to the production of CO in the exhaust, although in this campaign only comparatively small levels were observed.
- There is some evidence to suggest that high levels of CO<sub>2</sub> diluent will more readily transport heat to the root of the flame and this could be the reason for slightly elevated NO<sub>x</sub> production.

# Impact

- The data shows that despite very different physical properties between the diluents, under the conditions tested, stability is still largely governed by velocity distributions in the central recirculation zone.
- Thus for CO<sub>2</sub> moderated flames, existing swirl burner design rules can be modified.