



Cambridge Carbon  
Capture



***Mg(OH)<sub>2</sub> (& high-value by-products)  
from Serpentine & Olivine for  
scalable low-energy wet-scrubbing  
of CO<sub>2</sub> from ambient air & flue-gas***

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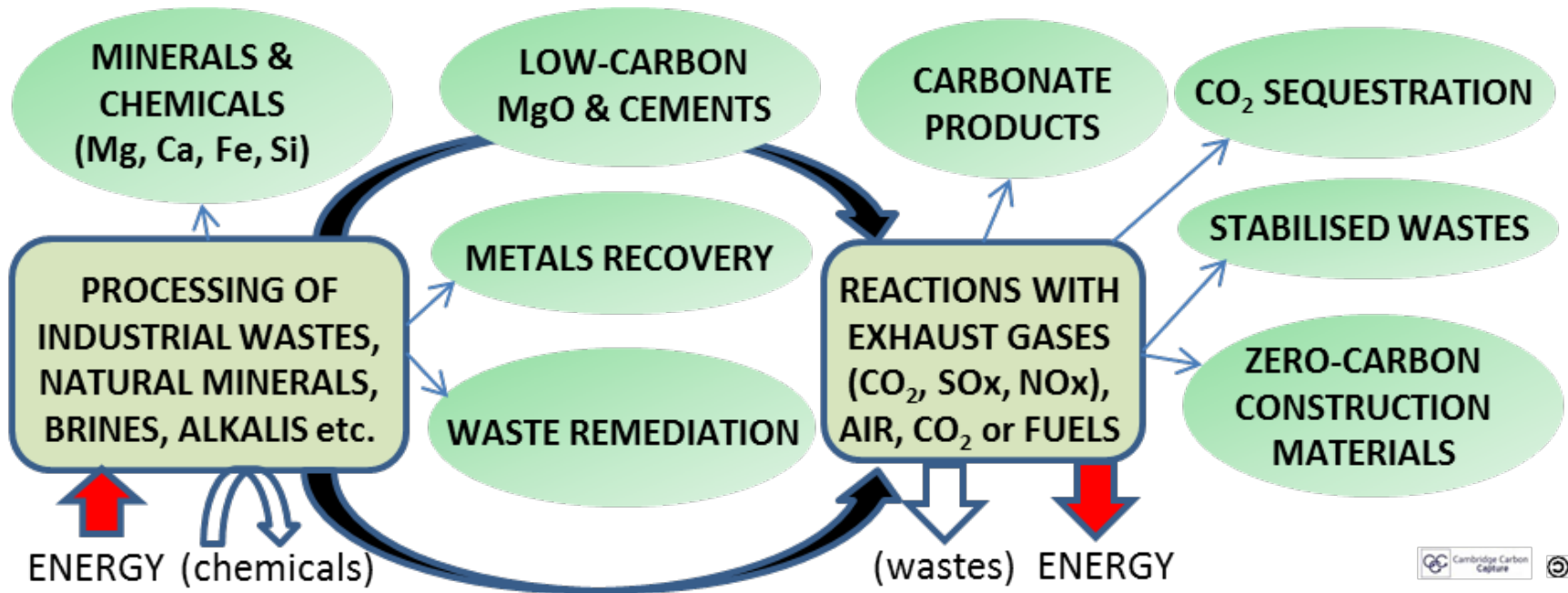
“Alternative Pathways to CCS”, Oxford, 26<sup>th</sup> June 2014

*CCC is a Cambridge-based, early-stage venture company developing a unique, profitable Mineral Carbonation process to sequester flue-gas CO<sub>2</sub> directly & permanently as magnesium carbonates.*

# Presentation overview

- **Scalability of mineral carbonation – what's needed**
- **CCC processes – our approach to scalability**
  - *Serpentine/Olivine-to-Brucite*
  - *Direct wet scrubbing of low pCO<sub>2</sub> - Brucite-to-carbonate*
  - *Energy recovery from carbonation*
- **Mineral carbonation on ships – overlaps with ocean liming**
- **Messages from MC community to policy makers ?**

# Where does MC fit – CCS or CCU? Niche business or large-scale ?



Alcoa: red mud waste stabilisation



C8S: APC wastes to building blocks



CCC: olivine-to-Mg(OH)<sub>2</sub> & SiO<sub>2</sub> for scalable CCS

# What needs to be done (for scalability) ?

- **Life-cycle process optimisation**

- process improvements to minimise energy & chemical inputs needed to activate minerals
- react directly with low- $p\text{CO}_2$  exhaust gases (not pure  $\text{CO}_2$ )
- Reliable, appropriate, consistent methodologies for LCA

- **Scale processes & business case for gigatonnes of  $\text{CO}_2$**

- process energy minimisation
- recovery of carbonation energy
- product & process development for profitable integration into large-scale construction materials sector
- recovery of valuable trace metals from mineral feedstocks

# CCC process schematic – digestion step 1

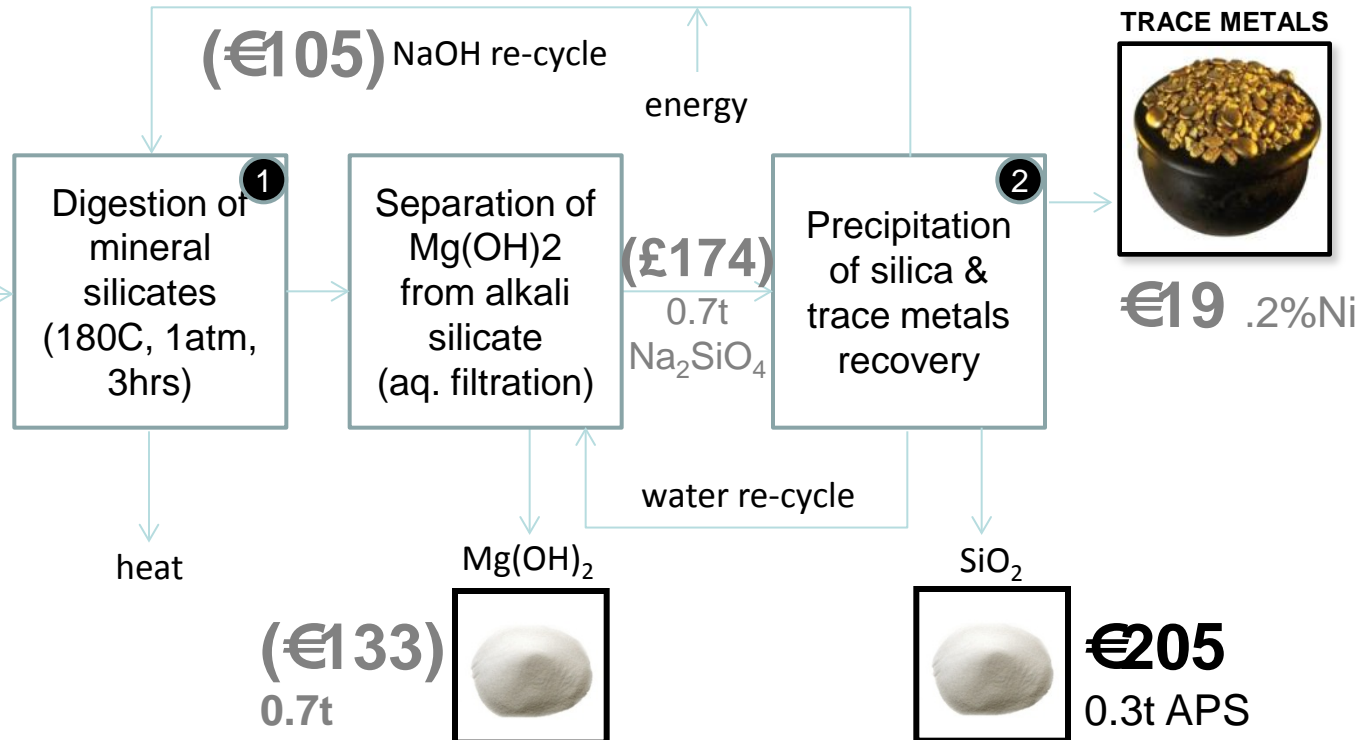
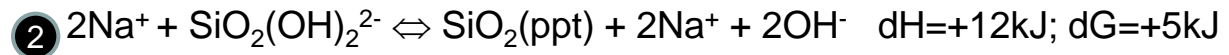
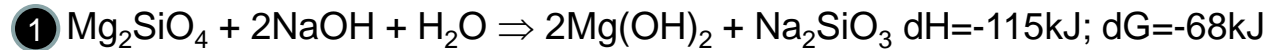
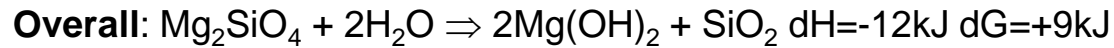
(alkaline digestion of serpentine or olivine to convert to brucite & silica)

**USP: profitable, low-energy, silicate digestion process**

PROCESS COSTS:

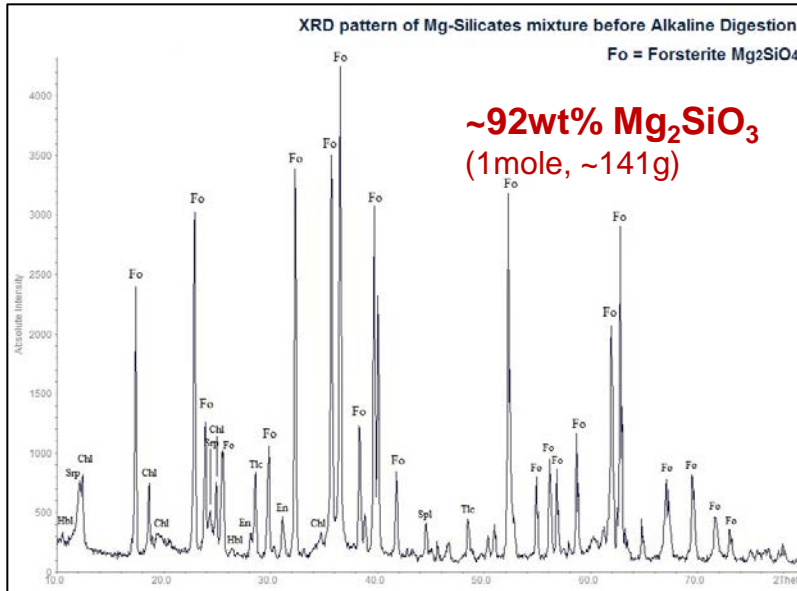
**€12** 0.8t olivine

**€105** 0.5t NaOH  
(/tCO<sub>2</sub> sequestered)

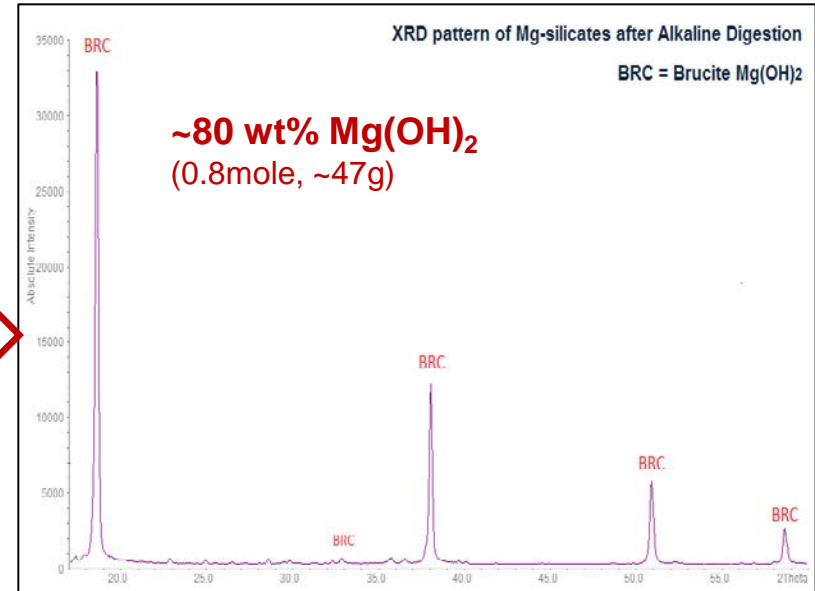


# CCC Process: Olivine-to-Brucite conversion at high-pH

Before Digestion



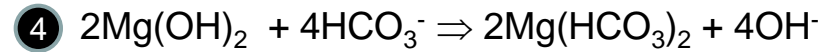
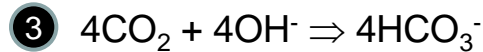
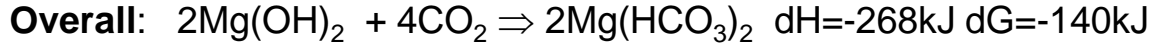
After Digestion



single-step, fast, low-energy conversion of  
magnesium silicate to magnesium hydroxide  
e.g. low-carbon alternative to portlandite

# CCC process schematic – carbonation step 2

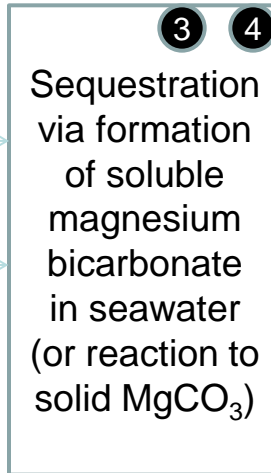
(direct carbonation of brucite (magnesium hydroxide) with flue-gas into ocean or products)



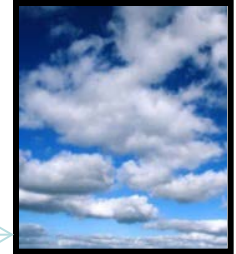
Diesel exhaust



$\text{Mg}(\text{OH})_2$   
(€133)  
0.7t



decarbonised  
flue-gas



€35 1t  $\text{CO}_2$

$\text{Mg}(\text{HCO}_3)_2$  SOLUTION



Heat, or  
CARBON-FREE  
ELECTRICITY  
via FUEL CELL



...alternatively,



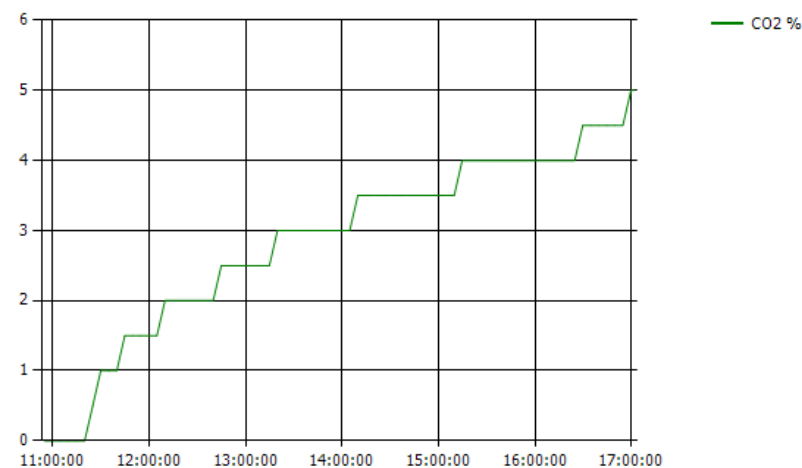
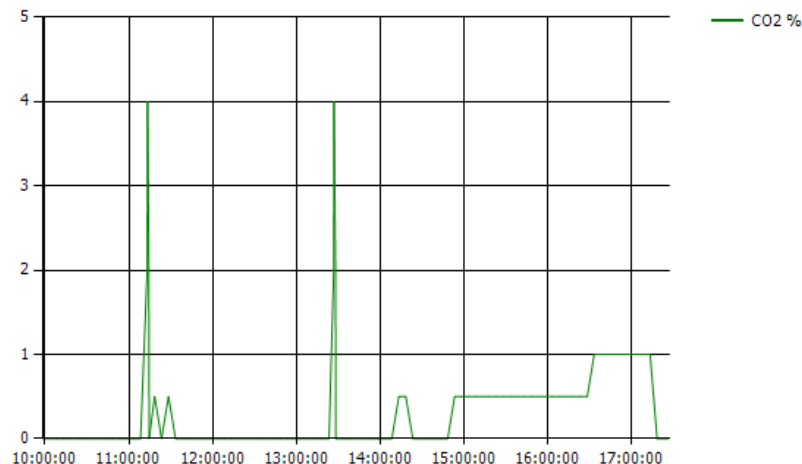
$\text{MgCO}_3$  Powder  
€192 1t

USP: “zero-carbon”, “zero-cost”  
permanent  $\text{CO}_2$  capture & storage



# Wet carbonation: Brucite-to-bicarbonate (5% CO<sub>2</sub>, rtp)

5vol% CO<sub>2</sub> inlet; 0vol% CO<sub>2</sub> outlet  
2.25 litres/minute  
Ambient Temp. (11C) & Press.(1atm)  
0.1 molar Mg(OH)<sub>2</sub>  
10litres recirculating liquid

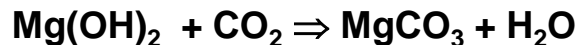




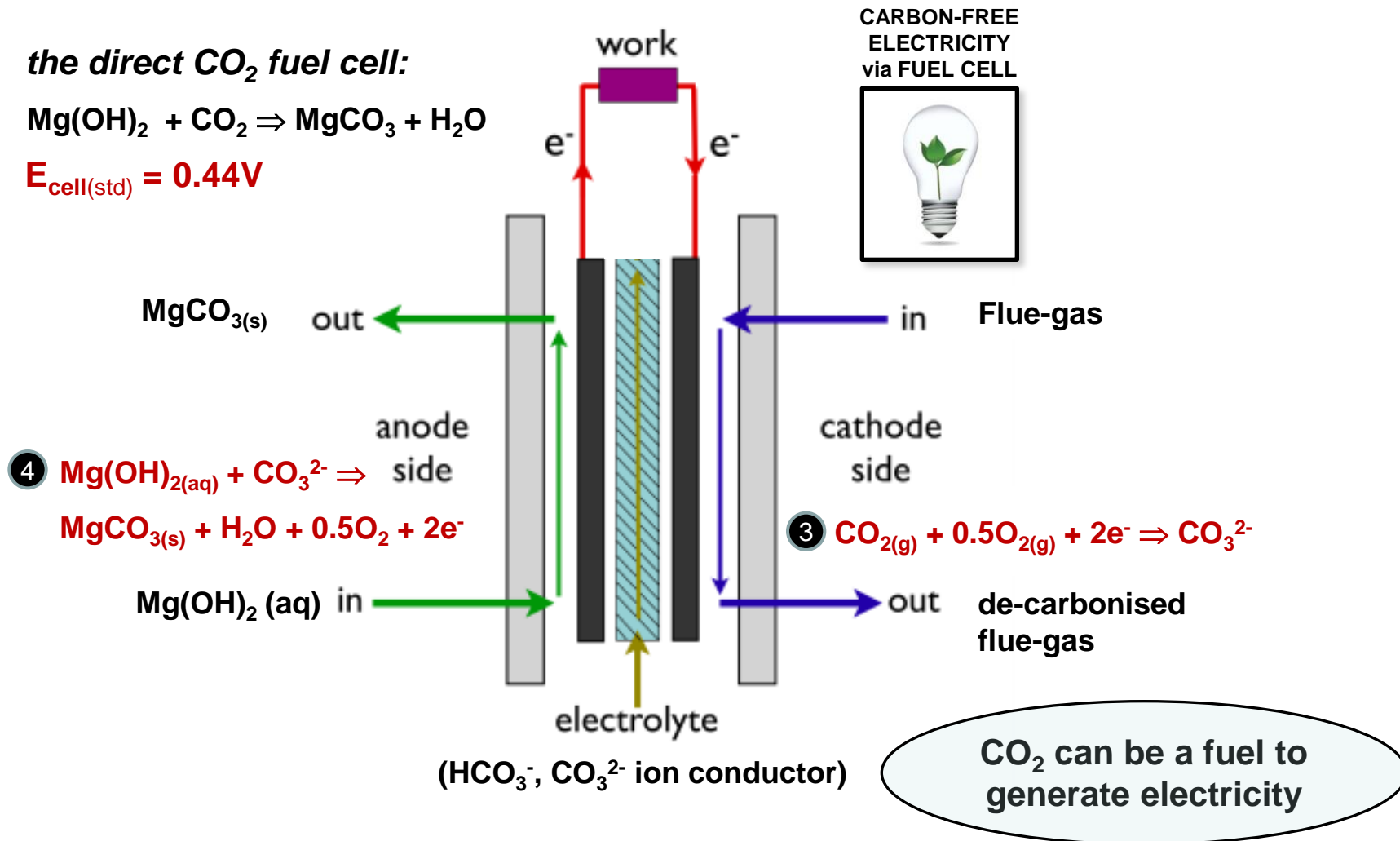
# Electrochemical Mineral Carbonation – option for carbonation step 2

(energy of carbonation recovered as carbon-negative electricity via direct CO<sub>2</sub> fuel cell)

*the direct CO<sub>2</sub> fuel cell:*



$$E_{\text{cell}(\text{std})} = 0.44\text{V}$$



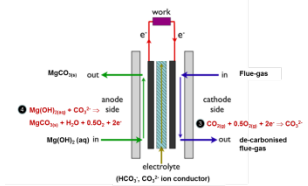
# Key R, D & D Challenges – considerable work still to do

- Process engineering design to offset process energy inputs against reaction energy outputs
- LCA to accurately assess net energy usage/output, net CO<sub>2</sub> sequestered
- Assessment of capex & opex – expert engineering design studies & demos needed to answer
- New processes that maximise kinetics of both activation of feedstock minerals and of carbonation while minimising energy/chemicals inputs; and avoiding creation of any wastes
  - Modelling of thermodynamics & kinetics of process steps
  - Particular energy intensity issues: evaporation of solvents; crystallisation/recovery of chemicals; sequential consumption of acids and bases
- Electrochemical approaches for both recovery of carbonation energy and chemicals recovery
- Development of processes optimised to use flue gas directly rather than pre-captured CO<sub>2</sub>
  - More research to investigate kinetics and thermodynamics in gas-solid and aqueous phase carbonation of magnesium silicates, (hydr)oxides and salts at low pCO<sub>2</sub>
  - Effects of flue gas impurities on product qualities
- CCSM potentially involves huge volumes of materials – better understanding of materials qualities, market requirements, volumes and prices needed versus MC process options
  - Processes optimised for different feedstocks
  - Processes optimised for different product outputs
  - Research on effects of seawater as solvent system for large-scale CCSM
  - Processes optimised for different market applications and scales of operation
- Much greater funding needed for interdisciplinary R&D and for multiple commercial demos
  - Process concepts need to be reduced to engineering practice and evaluated at pilot scale
  - Disparate R,D & D activities currently, due to sub-critical, fragmented sector, needs coordination and investment to develop a critical mass of activity; dedicated conferences and journals needed

# A blueprint for implementation & scale-up

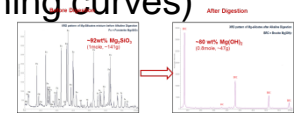
## 1. Multiple low-cost demonstrations of industrial $\text{Mg}(\text{OH})_2$ carbonation *NOW*

- Use first in hardest, highest-value industry applications where geo-CCS not suitable
- Commercial  $\text{Mg}(\text{OH})_2$  exhaust gas cleaning systems are available to strip low- $p\text{CO}_2$  into seawater solution or solid carbonate, using natural mineral brucite
- Multiple demonstrations to get the 22% cost-reduction learning curve underway
- future R&D on direct- $\text{CO}_2$  fuel cell to recover 0.5MWh electricity per tonne  $\text{CO}_2$



## 2. R,D&D support to energy-minimise available serpentine-to-brucite/ $\text{Mg}^{2+}$ processes

- e.g. CCC's single-step olivine-to-brucite process; other acid/alkali multi-step processes
- Demo with expensive natural brucite, transition quickly to cheap serpentine-derived brucite
- Support for multiple demonstration of commercial serpentine process plants (learning curves)
- policy support needed for non-electricity  $\text{CO}_2$  sequestration (including from air)



## 3. R&D support to optimise large-scale feedstock processing for by-product recovery of high-value critical metals and advanced industrial minerals

- to provide a sustainable revenue model for large-scale mineral carbonation; work with mining ind.

## 4. R,D&D support & policy intervention to integrate/substitute carbonated products into the high-volume construction materials sector

- Policy support to introduce new low-carbon construction materials to a highly-traditional sector
- Value & uses for large-scale MC products essential to minimise carbon pricing

# KEY MESSAGES about CO<sub>2</sub> mineralisation

## Get the support & enabling policies right & Mineral Carbonation can deliver:

- Commercial deployment of industrial CO<sub>2</sub> sequestration, with potential for giga-tonne CO<sub>2</sub> scale
- Learning-curve cost reduction through market-driven volume deployment with no/low carbon price
- Economically viable distributed CCS(M) across the range from car & ships to industry & power
- MC opportunity is more about a disruptive alternative to (G)CCS than “using” CO<sub>2</sub>
- Without targeted R,D&D & policy support, commercial MC will remain niche & not reduce CO<sub>2</sub>

## Situation today – already commercially niche deployed, but in the very slow-lane:

- Niche commercial deployment based on materials valorisation models (even paying for CO<sub>2</sub>), but very few investors or customers willing to engage with development costs & technical & commercial risks
- Multiple technical approaches with different business models – dangerous to pick “winners”
- Commercial developers & academic researchers are starved of R,D,D&D funding
- Major R&D questions still to be addressed – “downhill” process, but CO<sub>2</sub> LCA uncertain
- Increasing academic research, but weakly coordinated & communicated, & little funding

## Next-step needs – demonstration funding & industry-academia R&D collaboration:

- Multiple FOAK & NOAK commercial demonstrations required (lots of small projects)
- R&D agenda defined bottom-up by industry needs rather than by top-down CCS policy – economic viability first; CO<sub>2</sub> LCA viability second; large-scale CCSM third
- More interdisciplinary R,D&D collaborations; industry partnership critical; funding is critical – process chemists, engineers, modellers, geochemists; mining, metals, minerals, cement, steel, waste, chemicals
- R&D & industry network needed to improve knowledge sharing; more R&D centres = more processes
- Level the playing field with geo-CCS (MC is generally outside scope of CCS programs)
- Policy mechanisms needed to valorise CO<sub>2</sub>-sequestration independently of emissions reductions

***“CCC objective: profitable solutions for industrial customers to valorise ultramafic minerals & wastes and to permanently sequester CO<sub>2</sub> via conversion into valuable minerals, metals & zero-carbon electricity”***



- University of Cambridge – Depts Materials Science & Metallurgy; Engineering
- University of Nottingham – Centre of Innovation in CCS
- University of Sheffield – Dept. Materials Science & Engineering
- University of Greenwich – School of Science

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